Mars Space Construction, LLC

<u>CONTENTS</u> <u>PIPE STRESS ANALYSIS & PIPE SUPPORTS</u>

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Section 12

PIPING STRESS ANALYSIS AND PIPE SUPPORT DESIGN

12 . 1 INTRODUCTION

Piping systems are used as media of rt anspol·ting process and utility materials in various plant operations. The materials can be gaseous, liquid, or in the form of pellets, powder, or slurry. In all cases, an internal pressure differential or change in the elevation of the piping is r quired to move the material inside the pipe from one point to another. The material can be hot, cold or near atmospheric temper a.tures. Loaas acting on the piping are from the weight of the material being transported, the weight of the pipe, and the insulation of the system itself including such concentrated loads as valves, flanges, strainers, in-line pumps and various other similar components. External forces which act on the piping can be from wind or ear th-quake and induced reactions from mechanical vibrations.

All of the above loadings d velop restraining forces within the wall of the pipe itself, The intensity of this force related to the area of metal to which it is appli d (i. e. pow1ds

of force per square inch of area) can be referred to as the "stress" acting at a particular section in the pipe. The maximum stress permitted to act on piping within refineries and chemical plants is governed by a "Code for Pressure Piping" known as the ANSI (American National Standards Institute) B31. 3-1973. The procedure used to determine the stress levels is a stress analysis.

12. 2 STRESS ANALYSIS

12. 2. 1 General

Two basic types of stress analyses are performed on piping systems: (1) the piping mate ials group prepares specifications which give wall thickness requirements to withstand certain pressures and temperatures within code-allowable stresses; (2)the piping flexibility analyst, commonly called the "stress analyst, "reviews all piping for expansion and weight-induced stresses and other miscellaneous stresses.

12.2.2 Stress and Strain

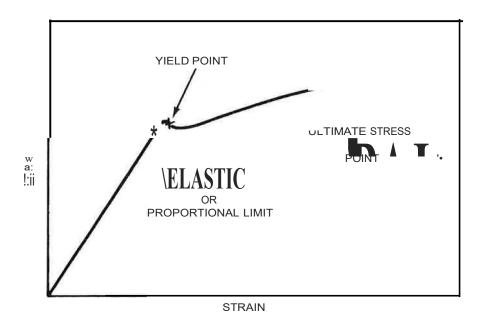
As previously mentioned the intensity of a force (F) actin g on an area (A) is known as the unit stress and is commonly expressed in (pounds per square inch or psi):

Unit Stress
$$(S) = \overset{F}{A}$$

When a system undergoes an applied stress it elongates or compresses. The total elongation or compression, call it (4), divided by the total length (L) of the body is known as the unit strain.

Now, it is known that the relationship of stress to strain is ganerally constant for most materials, that is $\frac{STRESS}{STRAIN} = E$. This is known as Hooke's Law.

Figure 12-1 shows an idealized stress versus strain relationshlp.



F i gur e 12-1. Idealized Stress versus Strain Relationship.

- (I) Up to the proportional limit, as stress (or load) is increased, the strain (or elongation) increases linearly,
- (2) When the stress exceeds the elastic !unit the strain increases at a greaterr ate; the material then becomes permanently stretched and will no longer behave in a per fectly elastLc manner.
- (3) As the stress is increased fur ther, the member elongates abnormally until the maximum stress withstood by the member is achieved. This is called the ultimate srt ength of the material.
- [4] If load is maintained on the member after the ultimate stress is reached, the member continues elongating until it breaks.

For future reference, the yield point and ultimate stress are synonymous with yield strength and ultimate tensile st ength. The value (E) is known as Young's Modulus and is generally a constant, below the stress whe.re yielding of the material occurs. The value of the constant (E) for some piping materials at 70°F is:

MATERIAL	E
Carbon Steel	29, 9 x 10^6 pSl.
Stainless Steel	28, 3×10^6 psl.
Alumim11n	'10, 6 x 10 ⁶ psi
Copper	16.0 psi
Cast Iron	13.4 psi

As the temperature of a material increases the value o E decreases, meaning that less stress is required to produce a given strain. As a material gets colder just the opposite is true, at least to temperatures down to low atmospheric.

12.2.3 Types of Stress

MATERIAL

Themanner in which a force or load is applied to a pipe determines the type of stress it undergoes. The types 0£ stresses that are most commonly dealt with are tensile, compressive, shearing, and bending stresses andare shown in Figure 12-2.

To show actual stress and strain values assmne that L = 100 inches, F = 1000 pounds and the member stressed is a 6-inch, schedule 40 pipe (area of metal cross-section = 5, 58 sq. in).

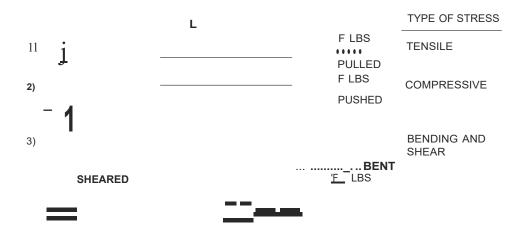


Figure 12-2. Examples of Types of Stresses

For tension or compression:

UNIT STRESS =
$$\frac{F}{A}$$
 = $\frac{1000}{5.58}$ = 179. Z p s i

UNIT STRAIN - $\frac{\text{Unit Stress}}{\underline{E}}$ = $\frac{179.2}{2^{\frac{9}{5}}}$ $\frac{2}{5}$ 10 6 = 5.99 x 10 in. in.

TOTAL STRAIN (.1) = L x UNIT STRAIN

= 100 x 5.99 x 10 -6 = 0.000599 inch

To evaluate shearing stress, the area of metal being shear ed laterally is the sani.e as for tensile stress, therefore the F indicated shear stress is the sarn.e, since $S := A^{\prime\prime}$

In order to evaluate bending stress wemust determine a bending moment (M) in the pipe and a special property of the pipe cross-section called section modulus or "Z." The formula for bending stress is SB= where Z can be obtained for every pipe size from piping catalogues such as in Tube Turn. It is beyond the scope of this program to explain section modulus but bending moments should be further clarified. Simply stated, when a force acts sideways on a member to cause it to bend the force causes a "bending moment" to act on the member. This moment varies proportionately with the size of the force and the distance from the point on the member where the force is applied. This relation is shown by the formula M = FX where X is the distance to a point where the bending stress is desired from F, the applied force. From the formula for bending stress previously given it is apparent that the maximum bending stress occurs at the location of the maximum bending moment or where X = L. FL The bending stress is SB=Zand Zfora6-inch schedule 40 pipe is 8.5 in.,

$$\frac{1000 \times 100}{8.5} = 11, 765 \text{ psi}$$

In preparing a piping specification, the wall thickness of any size pipe generally depends on a limiting pressure and temperature combination. The stress in the pipe wall due to

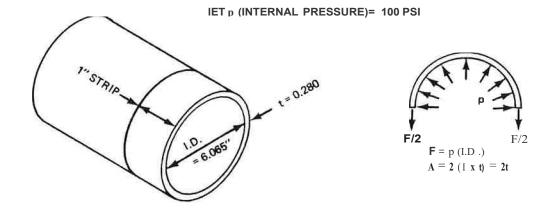


Figure 12-3. Hoop Stress from Inte nal Pressure.

internal pressure is a tensile stress and is commonly called hoop stress. Its value is calculated as follows.

F = 6. 065 x 100 = 606, 5 lbs
A = 2 x 1 x 0. 280 = 0. 56 sq. in.
S =
$$\frac{E}{A}$$
 = $\frac{606}{0.56}$ = 1083 psi

Without corrosion allowance this pipe would be within the code-allowable stress at about 1050°F.

12.2.4 <u>Allowable Stress</u>

When a stress analysis of a piping system is completed the maximum stress of the system has to be compared to what

is known as the allowable stress permitted by code (ANSI B31. 3).

The allowable stress depends on the material the pipe is made from and the maximum service temperature that it will be subjected to. The allowable stress is determined as the lowest of the .following:

- (1) 1/3 of the ultimate tensile strength
- (2) 2/3 of the yield strength
- (3) The stress producing a creep rate of O. 01 percent in 1000 hours
- (4) 67 percent of the average stress producing rupture in 100,000 hours (roughly eleven years of continuous operation)
- (5) 80 percent of the minimum stress producing rupture in 100,000 hours

Allowable stresses also depend on whether the stress is primary (sustained) or secondary (self-limiting). An example of a sustained stress is onecaused by weight or internal pressure. A self-limiting stress is onecaused by thermal expansion. The allowable stress for sustained stresses is

that for the basic material as previously described while for thermal expansion or flexibility it is roughly 1.5 to 2.5 times as much. For piping flexibility though, the allowable stress is really a stress range, This means that any prestressing of a piping system by cold springing uses uppart of the allowable stress range, permitting only the remainder to be useful in comparing it to the final hot expansion stress. This will be discussed further later.

23 THERMAL EXPANSION

As a pipe is heated from normal atmospheric temperature (70°F is used as the usual base for figuring expansions) to the service temperature, it expands, and, likewise when it gets colder it contracts. This is true for virtually all materials. Water and pr inte r¹s metal are twomaterials that do not follow this rule, since they expand upon cooling to the solid state. Expansion or contraction causes a piping system to be sprung between its end connections. The end connections are nozzles to pumps, turbines and compressors, vessels, heaters and air fans, or connections to other piping systems.

An example of a sprung piping system is shown in Figure 12-4.

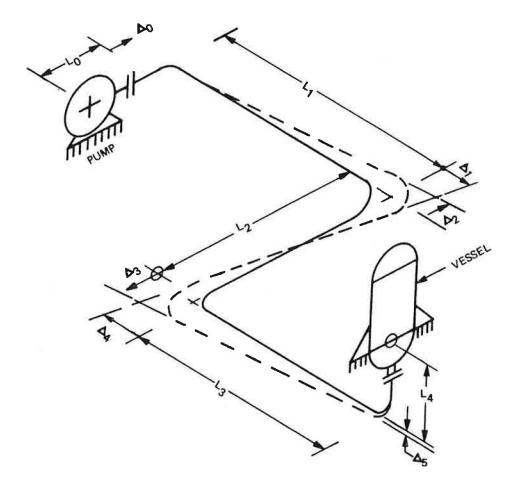


Figure 12 - 4.

As you can see, the various lengths have increased by the amounts shown by the synibol delta $\langle L \rangle$. These increases in length when restrained from free movement cause a bending of the pipe to occur and therefore induce bending moments and srt esses. The actual expansions Ll L, .12,

L13, etc., are computed by multiplying the lengths by the mean coefficient of expansion, Therefore, $\mathbf{L1} = \frac{\mathbf{L}}{100} a$, usually **L1** is calculated in inches, L is the length of pipe in feet, and a is in inches per 100 feet,

2 REACTIONS ON EQUIPMENT

Restraint of free thermal expansion induces reactions such as forces and bending moments in the piping and on equipment. Not only is it imperative to limit bending stresses in piping to the allowable, but reactions on equipment, es - pecially rotating equipment, must be limited as well.

Reactions on equipment are often limited by published loads on manufacturer's drawings. Where allowable loadings are not given, it is up to the judgment of the stress analyst to limit the loadings by rules of thumb developed through years of successful application. Equipment that require close scrutiny of imposed loads are: pumps, turbines, compressors, air fans, and heaters. The stress analyst usually prepares calculations for pipe reactions on all rotating equipment operating above 250°F. Stresses in piping systems connected to equipment that are sensitive to reactions also must be well below the allowable permitted because high stresses are generally caused by high reactions,

Sometimes the reactions on equipment can be reduced below the allowable by using cold spring. As previously stated, this method does not reduce stresses, because the stress range is merely shifted and not reduced by cold spring.

But the reactions are reduced since the final forces and moments are a function of the actual amount of system elongation being re strained. Moreover, if the total elongation is split up so that part of it is used to pre-deform the system then the deflection at either time from neutral position, during cold spring or final operation, is less than the total.

For example, if it takes 100 pounds to deflect a cantilever beam 1 inch, then if the 1-inch deflection is split into 1/2-inch cold spring and 1/2-inch final movement, the force to cold spring or cause the final movement would be 1/2 x 100 = 50 lbs, (See Figure 12-5.)

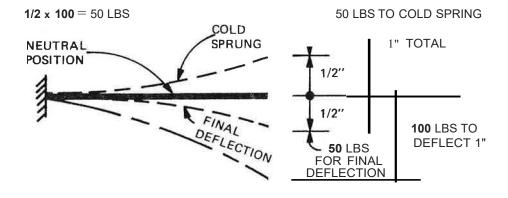


Figure 12-5.

12.5 FLEXIBILITY OF PIPING

For piping to absorb expansion or contraction within the Hxed terminals of a system the routing of the pipe must include at least one offset of sufficient length. A pipe cannot be routed in a straight line between to minals and yet absorb the effect of large temperature changes, The following example shows the forces and stresses set upby a straight pipe undergoing a temperature change.

Assume a 6 inch schedule 4-0 carbon steel pipe held between two fixed points 10 feet or 120 inches apart. If the pipe is heated up 100°F a compressive stress and reaction is set up. From formulas previously given

UNIT STRESS =
$$\frac{\text{Restraining}}{\text{Area}} = \frac{\text{Force}}{\text{A}} = \frac{\text{F}}{\text{A}}$$

UNIT STRAIN =
$$\frac{\text{Total Elongation estrained}}{\text{Total Length}} = \frac{\text{LI}}{\text{L}}$$

From E =
$$\frac{\text{UNIT STRESS}}{\text{UNIT STRAIN or -; } \vec{\Gamma} - := }$$
 All

Since
$$LI = LT$$

Then $E = \frac{F}{ALTa}$ F
And $F = AEaT$, where

o: = coefficient of expansion, in/in/°F
 T = total temperature change, °F
 L & E described before F, lbs,
 F, lbs.

NO TE: The restraining force does not depend on the length $^{"}L"$ of the system. Now by substituting,

F = S. 58 x 29.6 x
$$10^6$$
 x 6.5 x 10^{-6} x $100 = 107$, 300 lbs.
and S = $\frac{F}{A} = \frac{107300}{5.58} = 19,240$ psi.

Whereas the stress appears to be reasonable, although slightly higher than allowable, the reactive force is tremendous and would most likely' deform or break its attach.tne nt. For small temperature changes, if the total elongation is very small and can be tolerated by equipment deformation, a direct routing may be pe missible.

Since most equipment will only tolerate much smaller reactive forces and moments, piping must be routed with care to absorb the thermal expansion between fixed points. To evaluate whether a piping system is flexible enough, the stress analyst has seve all methods to approximate stresses

and reactions. The first method is crude and employs the equations of the simple and guided cantilevers.

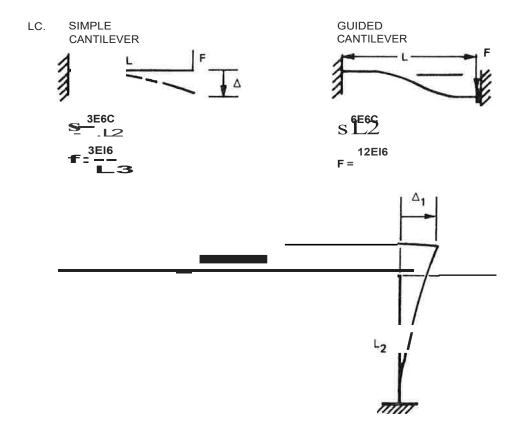


Figure 2-6

In the above example L_1 is adjudged to be similar to a guided cantilever deflected by $\mathbf{6.}_2$ and the length, L_2 , is close to a simple cantilever deflected by $\mathbf{6.}_2$. The formula is then applied

and the approximate stress andforce are calculated. Whatever assumptions are made, they should be on the conservative side. In recent years a better tool has been developed to give closer approximations. This tool is the "Table for Expansion Loop Sizing." Offse sin piping systems are compared to one -half of an expansion loop and the force and stress estimates are made by direct interpolation from the tables. The reason that the expansion loop table gives such a close approximation is because it employs the effect of pipe elbow flexibility. This elbow flexibility comes from the irnattening effect¹¹ of the elbow poss-section under an applied moment.

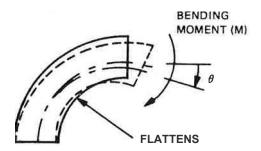


Figure 12-7

As the elbow flattens its moment of inertia or, let's say, measure of stiffness decreases. Therefore it can be thought of as a partial hinge. When two elbows are connected by a straight length of pipe, the total system becomes the major unit of flexibility in piping.

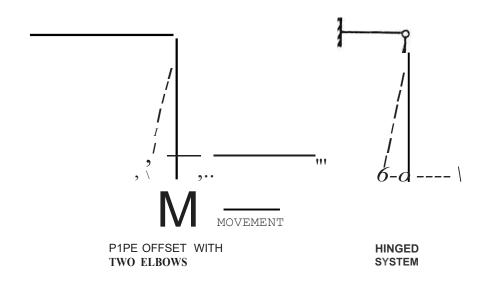


Figure 12-8. Closely Equivalent Systems.

The elbow itself absorbs some of the system elongation

" but generally only a very small per centage. Therefore, the system's flexibility is not increased gl"e atly by s imply adding elbows but rather by adding offs ts with elbows at each end. The rotation of each elbow linked together with

the straight pipe accounts fot- the largest percentage of the deflection 11.1"•

12. 6 STRESS RAISERS

When stresses ofpiping systems are calculated a special factor or multiplier must be included, This additional multiplier is called an intensification factor because the true stress is larger than the basic calculated stress due to a "stress raiser." Stress raisers may come from sharp reentrant angles such as at the junction of a stub-in tee to the main header or at the weld junctions of mitered elbow. When elbows flatten, a stress raiser also appears in the more sharply bent portions. These intensification factors can be computed by formulas in the B31. 3 code and are assigned the symbol "i".

The final stress at anypoint of a piping system is the calculated stress times this intensification factor. The smaller the radius of the elbow or bend the higher the "i". Mitered elbows have g eater i's than smooth elbows or bends. As the mitered ells have more sections, the i's will approach that of a smooth bend.

12.7 COMPARISON OF EXPANSION LOOPS AND TYPES OF ELBOWS

The force to deflect and the stresses induced in an expansion loop when absorbing movements from thermal expansion are not only functions of its size and shape but are also related to the type of elbows or bends used with in it. The following exa.inples show this relationship for two different pipe sizes.

From Figure 12-9 we can conclude that:

- (1) A given size expa sion loop with bends can absorb
 the greatest amount of expansion within the gi ven
 allowable stress. Thedrawbacks are that greater
 anchor force is needed and it is more difficult to fit
 into pipeways.
- (2) The expansion loop with 3- piece mitered elbows

 (Figure 12-9 C) may be used. Although its length

 may present difficulties, it can be shortened by

 making the elbow with 4, 5, or 6 mitered sections.

12.8 8 HOWTOIMPROVE FLEXIBILITY

Offsets. From previous discussions we have seen that expansions within a system between fixed points are absorbed by o.ffsets within the system. We also know that bending stresses and forces are re.Lated to the length of the offset

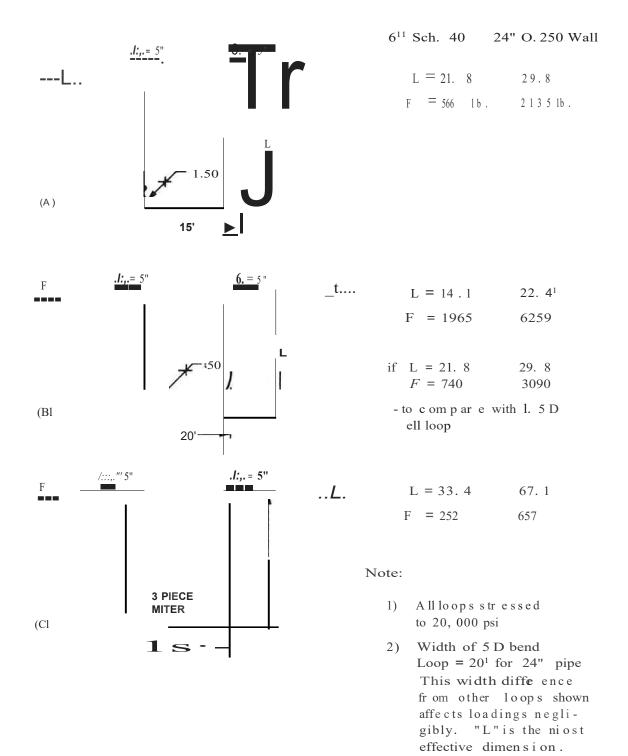


Figure 12-9

absorbing the move nt. These offsets, to be most *effi*cient, should be located at right angles to the imposed expansion or move nt.

(I) Single Pb.ne System

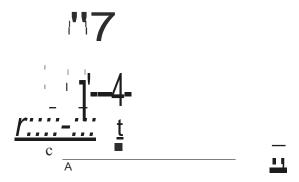


Figure 12-10.

- (a) Asswne that offset ¹¹B¹¹ is too short to absorb expansion of ¹¹A¹¹.
- (b) Adding loop " C^{11} is very ineffective in improving the flexibility of the system to absorb the expansion of "A".

(c) Adding loop "D" (at right angles to expansion of "A") is the most efficient means of improving flexibility.

(2) <u>Multi-Plane System</u>

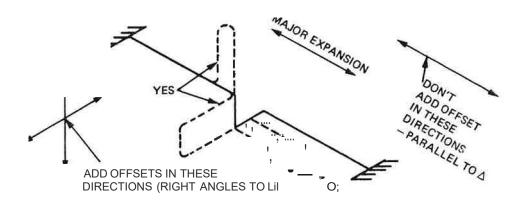


Figure 12-11.

12.9 EXPANSION ABSORBING DEVICES

If a piping system cannot employ offsets or loops to absorb expansion because of space limit ations, either expansion joints or couplings may be utilized.

(1) <u>Expansion Joints.</u> These are made up of flexible bellows or convolutions to contain pressure, yet,

allow £or axial movement or angulation. The draw-back to their use is that high anchor forces are required to contain the pressure force and spring force 0£ bellows. Tandem units, with tie-rods, at right-angle to movement provide a simpler solution.

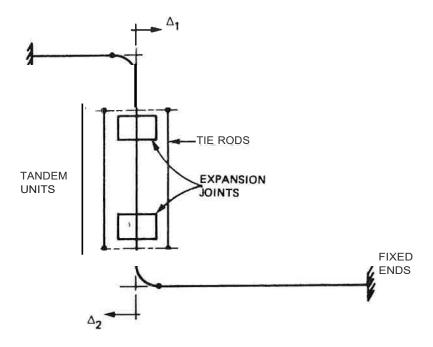


Figure 12-12.

Expansion joints are easily damaged from weld splatter which leaves pin holes, stress corrosion cracking from the

presence of chlorides, and mishandl ng. The convolutions generally are O. 032 to O. 062 inch thick and are made of stainless steel.

Couplings. Nor mally when couplings are used to (2) absorb equipment or pipe movements they are used in pairs as in the tandem unit of (1). Although small axial movements can be accommodated by couplings say, up to 3/8 inch each - their major use is in tankage areas or in cooling water lines where tank settlement and buried header settlement affecting connecting lines can be handled by the lateral deflection of a tandem unit. Dresser couplings and their equivalents may require tie rods across them to contain the pressure thrust. Victaulic and similar types of couplings are self containing, that is, their boltedon clamp fits into machine grooves in the end of each adjoining pipe to prevent blowing apart. The drawback of couplings is that their leak-proof integrity depends on rubber gaskets bearing on the outer pipe surface. Therefore, their use is avoided in hydrocarbon service, except in areas away rf om process units such as tankage areas.

12. 10 CONTROLLING PIPE EXPANSION

If a length of pipe resting on pipe supports is heated it tends to expand from its center toward each end, Now if this pipe starts at a pump discharge at one end and runs the full length of the unit's pipeway, say 400 feet, and operates at 350°F, the expansion of 1/2 of its length would be 4.6 inches, Obviously this expansion would create quite a problem around the pump. Therefore, to protect it from expansion, the pipe would be anchored in the pipeway near the pump and all the movement in the pipeway would be thrust into an expansion loop midway along the pipeway with an anchor near the far end of the pipeway to protect clearances between pipes.

The:rrnvements in interconnecting pipeways require control such that their expansion doesn't cause pipe interferences among lines entering from adjacent process units. (See Figure 12-13.)

Expansion of piping in pipeways can create clearance problems between adjacent branch lines connected to the pipeway, All branch lines are checked out for this interference as shown on Figure 12-14. Lines are never allowed to touch each other, therefore, after move nts, lines should have a minimum of 1-inch clear. Sometimes cold springing of

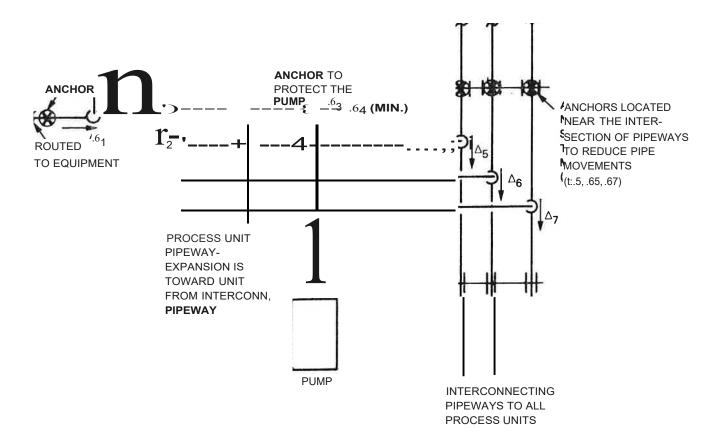


Figure 12-13.

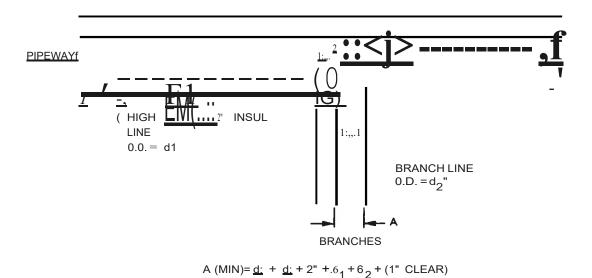


Figure 12-14,

branch lines can be utilized to provide the necessary clearanc,e For method and rotation of cold springing, see P.S.A. Standard C-723.

12. 11 DESIGN CONDITIONS AFFECTING PIPE FLEXIBILITY REQUIREMENTS

The following design conditions affect pipe flexibility requirements.

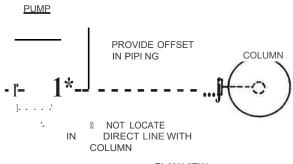
- (1) Normal operating temperatures
- (2) Upse t temperatures listed in line designation table column uncler EXP
- (3) Settlement of equipment foundations or pipe supports
- (4) Frost heave affecting foundations or pipe supports
- (5) Steam out of piping or equipment (usually taken at 300°F)
- (6) Steam tracing (usually taken at 300°F)
- (7) Wind loading
- (8) Earthquake effect
- (9) Buried pipe with temperature increase or decrease greater than say 20^{0} F

(10) Two-phase flow (slug flow)

12. 12 ELIMINATING STRESS PROBLEMS IN PLANT LAYOUT

The following objectives should be considered in order to eliminate stress problems during plant layout.

- (1) Ptunp locations relative to connected equipment See Figure 12-15
- (2) Routing of overhead vapor line to exchangers and air fans See Figure 12-15
- (3) Routing of connecting pipe from fractionating columns to strippers See Figure 12-16
- (4) Avoidance of direct routing of pipe bet\.veen equipnt - See Figure 12-16
- (5) Locating large heavy lines in pipeways near stanchion columns See Figure 12-17
- (6) Location of steam header in pipeway servicing turbines See Figure 12-17
- (7) Piping between pwnps operating at high temperature or subject to steam out, See P.S.A. StdC-732 (being prepared)



PLAN VIEW

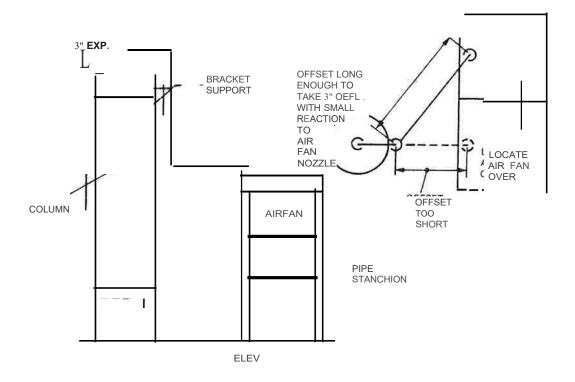
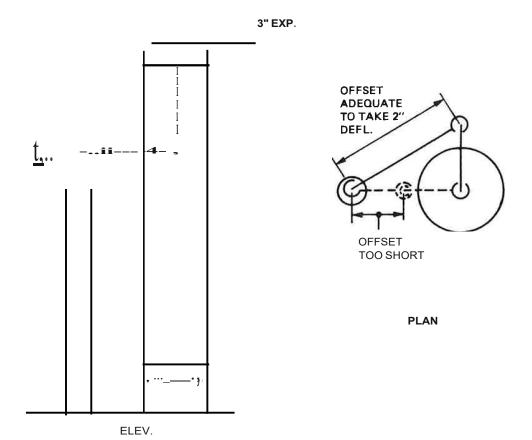


Figure 12-15.



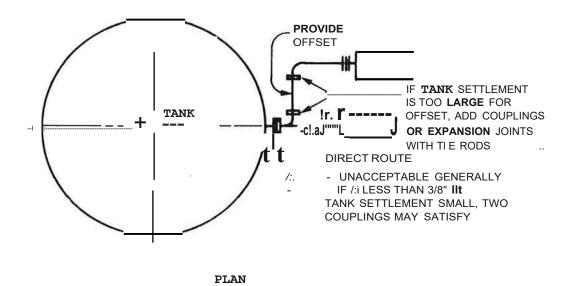


Figure 12-16.

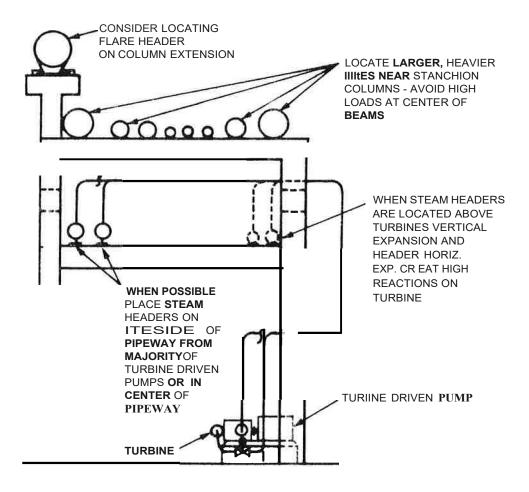


Figure 12-17.

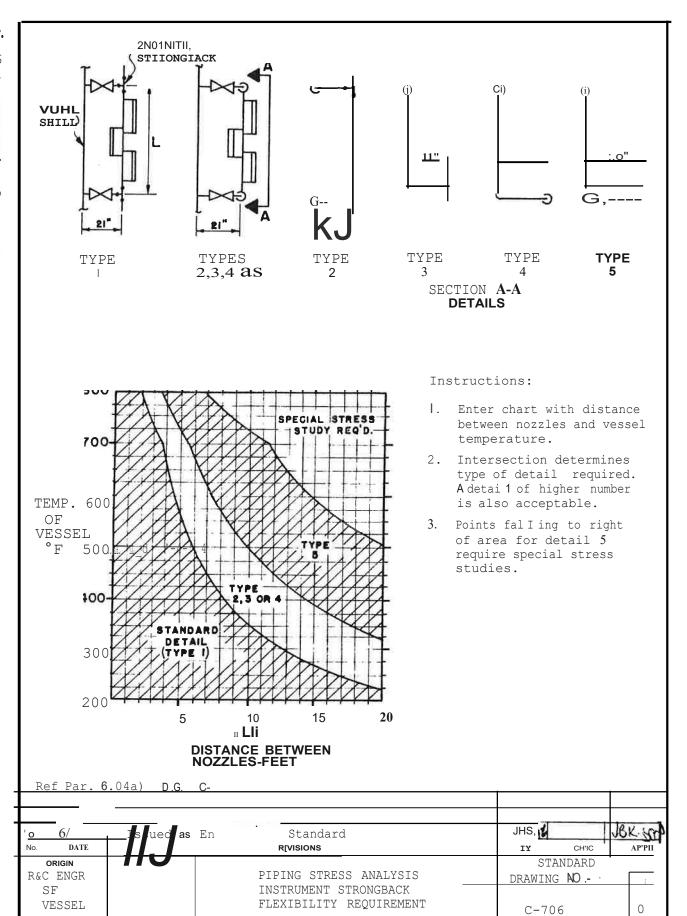
- (8) Piping inlet and outlet manifolds to airfans (See P. S. A. Std. C-717 and C-718)
- (9) Instrumentation piping on vessels (See P. S. A. Std.C-706)
- (10) Providing adequate clearance between branch lines to high temperature headers and adjacent branches to headers of other services See Figure 12-14
- (11) Stacked exchanger nozzle flexibility requirements See P.S.A. Std. C-715

<u>USEFUL PIPING STRESS ANALYSIS STANDARDS</u>

Standard support symbols '<;- 707
 Cold spring notations

 In-line purn.p supports
 Thermal expansion of steels

 C-723
 E-M-542 and 543



12-34

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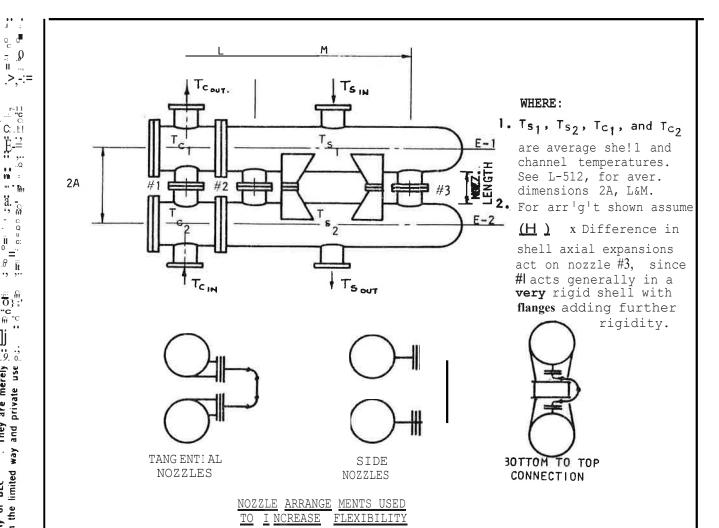
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SYMBOL 2	DESCRIPTION	COMMENTS
	Anchor	Axial Anchor only. Allows lateral movement. No description required with the symbol
15572 2	Guide	Stops lateral movement only or 1 imits movement. No description required with the symbol
25	Variable load	Used where <3" and load variation
TY 2552] 2	spring support	uQharmful.Give L
TYPE	Constant 1oad spring support	Used where 6.>3" and/or load variation harmful to system. Give $L'::$
67	Sol id, resting type, support	Any of several resting type supports
HUD	Single rod hanger	Any of several solid hangers. Deflection may be I imited. Give
12 H	Trapeze Hanger	Same as for H
A STAN	Guide Strut	If reactions greater than wind load, state amount. Give 's
A SHUTE	Hydraulic type Vibration snubber	Allows for slow thermal expansion. Give axial 1::: and max. reaction.
620	Vertical 1 ine guide	Give axia ${\sf I6}$ and direction of stop, if required
Thes s	Socket Guide	Give Vertical D

 $\underline{\text{NOTE:}}$ 6, • Pipe **expansion** or other induced movements

Ref	Psr.	7.16a)	D.G.	C-5
1				

71 1s c:.11 rl as	— Ennin,,rlnn C.tand	ar d			J			1,-,,
ATE	IIIVIItONI		IY	СНКІ		[NC. II	l'IIOJ (NCII	AP'PI
	D[SIGN[D	DIIAWN			«:liKJ" (NCI			
	DTDTMC Ç1	DECC AMAT	VCTC		JC>e No.	C.T II M n	ll r:Ht	
R	FIFTING SI	RESS ANAL.	1010			DIIAWINC	No	IIUI.
B	STANDARD SU	PPORT SYM	BOLS					0
L						c - 707		0
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NOTES:

1. Letting Tc = $\frac{\text{Tc}_1}{2} \pm \frac{\text{Tc}_2}{2}$ and Tsm = $\frac{\text{Tsl} + \text{Tsz}}{2}$ then if Tsm - Term 200°F and if Ts1 - Tsz < 100°F

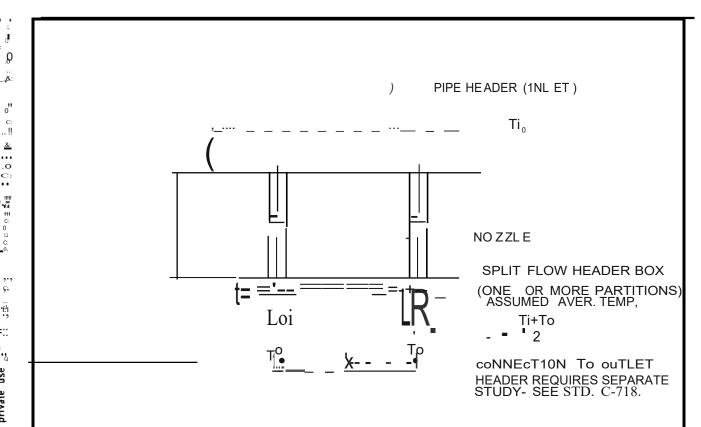
the exchangers may be directly connected per Std. L512 based upon past experience, but, if either is exceeded, the nozzle arrangement should be revised such that pipe elements can be included to absorb the differential expansions. Include in a piping flexibility calculation the 9pring constants of nozzle rotation from C-716. Neglect effect of saddle supports in calculation.

REF.:

- 1. D.G. C-5 Par. 6.08b) & 7,20b)
- 2. Ref. Eng. Std. L-512 "Dimensional Guide for Shell and Tube Exchangers"

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OR R &	RIGIN C	₽.al	PIPI	ING STRESS ANAL			JOI No.	STAN D		REV,
PRES VES		BECHTE		STACKED CACHAN NOZZLE FLEXIBILI REQUIREMENTS	_			C-71	5	





DESIGN BASIS:

- I. WHERE TOTAL DIFFERENTIAL EXPANSION (.6.) OF THE AIR FAN HEADER BOX 8 PIPE HEADER BETWEEN NOZZLES (XFT) IS 4S OR LESS, "J..." MAY BE FITTING MAKEUP.
- 2. WHERE !J.. IS GREATER THAN 16, THE MINIMUM LENGTH OF "y _"

 MAY BE CALCULATED BY THE FOLLOWING FORMULA:

 WHERE: E= 30>< 10 PSI (C.S.)

$$\ell = \sqrt{\frac{6E}{S}} \times \frac{-vM}{2}$$

S= 60,000 PSI (C. S.) t::,.• EXPANSION BE-

TWEEN NOZZLES-IN.

j = 27 (INCHES)

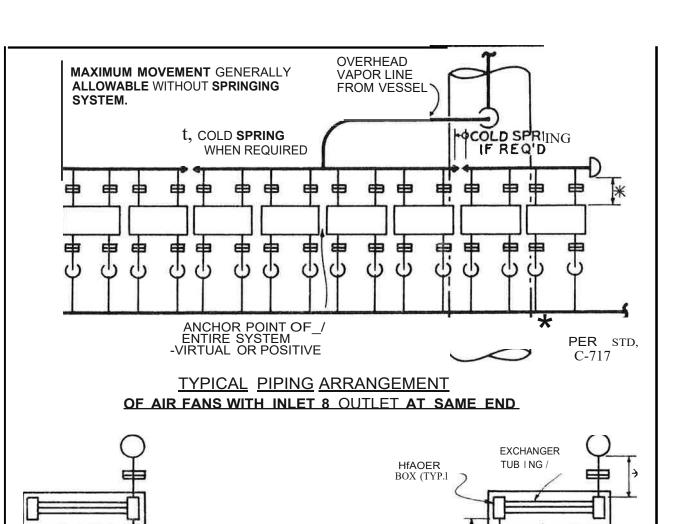
D= 0.D. OF PIPE-IN.

NOTE:

SIS BASED ON THE ALLOWABLE TOTAL STRESS FOR 1000 CYCLES OF STRESS REVERSAL FOR **CARBON** STEEL **(FROM ASME** SECT. EII, DIVISION 2)- REDUCED BY 23,000 PSI TO ALLOW FOR PRESSURE, STRESS **RAISERS**, ETC.

Ref Par. 5.41 D.G. C-5

Rel Par.	5.41 D.G. C-	-5							
									, ■•,
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ORIGIN		PI	PING STRESS ANALY	ISIS		JOI No.	i:::TA	InAlln	
R&C ENGR	12.33		AIR FAN COOLE		ļ		DRAWING	No	IIEV,
S.F. Vessel	BECHTEL		NOZZLE LENGTH COMPUTATION	[C-71	17	0



TYPICAL PIPING FOR AIR
FANS WITH INLET a OUTLET
AT SAME END

FOR

TYPICAL PI PING FOR AIR FANS WITH INLET & OUTLET AT OPPOSITE ENDS

SIOE SUPPORT

CHANNEL

OVERALL LENGTH OF AIRfi UNIT

NOTE:

- I. When pipe header expansion exceeds amount specifically permitted by air fan design, cold spring header to provide additional clearance required.
- 2. When nozzles are at same end of air fan provide flexibility to one pipe header as shown.

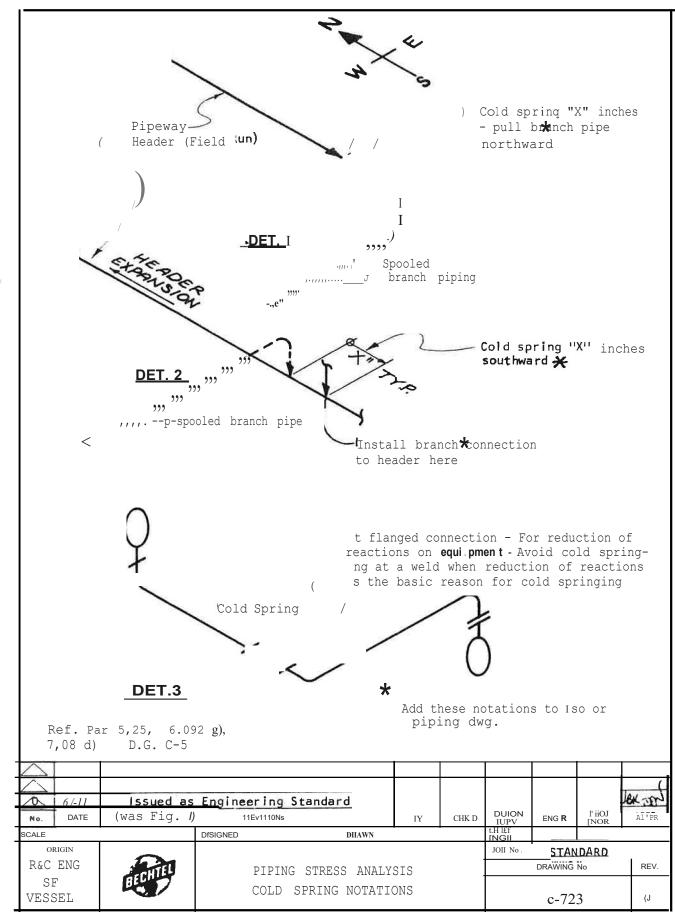
PER SPECIAL FLEXIBILITY

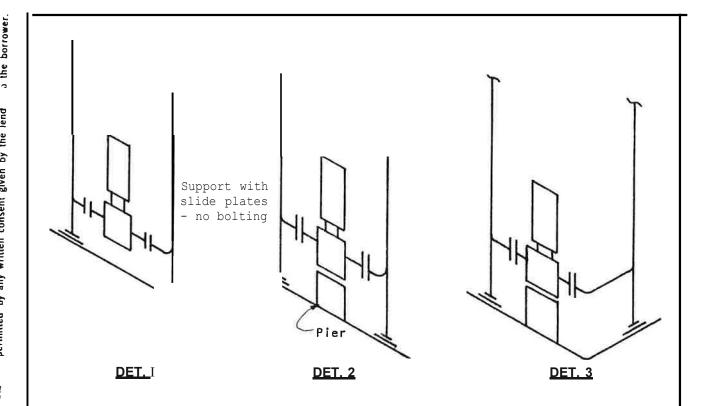
CALCI,!LATIONS AS REQUIRED

INLET- 6.ouTLET.

3. . When inlet & outlet are at opposite ends use minimum nozzle length permitted by C-717, Ref Par. 5.43 D.G. C-5

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S,F, Vessel			DE	SIGN				C-718	ı	0





Notes:

- I. Where the in-I ine pump horsepower is $75 \, \text{H.P.}$ or less use method shown on Det. I.
- 2. Where in-line pump horsepower is greater than 75 H.P. use method shown on Det. 2.
- 3. Where piping is eccentric, support as shown in Det. 3.
- 4. Where frost heave will affect piping detrimentally put all supports on foundations extending below the frost line.
- 5. Previous investigations have shown that earthquake loadings on typical systems are acceptable.

\Leftrightarrow									+
4 6/71	Issued as E	ingineering Standa	rd			JMS	8mx		Jen i
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D.G. C-5 Ref. Par. 5.105 ε 6.05

Carbon Steel (C.S.) • Carbon-Maly Steel - Low Ghrome Steels (thr..i 3% Cr.' 1. Notes, Low Chrome (L.Cr.) • Intennediate Alloy Steels (5% Cr. Mo. thru 9:t Cr.Mo. high Chrome (H.Cr.) .. Straight Chromium Stajnless Steels; 12% Cr. 17% Cr. 2. and 27 Cr. EXPAHSION IN "/1001 OF OF C.S L.Cr H.Cr ίΗ.er. OF C.S L.Cr. H.crJI C.S. L.Cr 4.0 4.1 4.2 1.1.2 4.3 4.4 7.4 7.5 8. 9.0 570 80 11000 1. 10 3.7 e.1 8.2 0.3 1)0 0.3 003/ 20 30 J:8 20 4:-1 0.4 0.s 4:5 7:9 o.h 688 8.₽ f 8:5 9.2 4-3 4.4 4:8 4:9 8.5 7.98 80 0.8 0.7 9:9 190 #0 9:5 4:5 4:7 e.; 0.9 0.9 *38* 4:9 4:24 4:3 9:6 200 90 €. ℃ 8.0° 10 20 80 9.8 8.9 8.1 1.1 1.0 50 5.1 t 60 4.8 t 4.4 9.9 30 1.2 90 9.0 5.2 8.2 1.2 1.1 1100 **1**10.0 **1**10.2 9.1 8.J 5.3 4.9 4.5 1.J 1.3 1.1 70 40 9.2 e.4 5.0 10 50 1.3 1.2 80 5.4 4.6 1.L 90 9.2 1.J 4.7 20 i 10.3 5.5 5.5 5.1 60 1.s 1.4 1110 054 f 9913!}8.1 ?D0 4.8 B0 80 1.7 5.2 1.5 104 50 B 9.5 8.8 5.8 90 1.7 1.6 1.5 20 5.3 4.9 50 \ 10.6 4300 110.8 9.67 1.6 6:0 5.0 60 8.89 1:8 2:0 1.8 5.5 JQQ 20 1.7 6.2 5.6 5.2 80 110.? 9.8 9.0 50 109 ! 11.0 9.9 9.1 5.7 5.3 90 1.e 1.9, 6.J 30 2.1 2.0 60 6.4 5.8 5.3 1200 11.1 | 10.0 11.2 | 110.1 9.2 2.2 2.0 70 40 9.3 2.1 10 1.9 80 6.5 5.9 5.4 50 2.3 20 110.2 ; 10.3 2.0 9:4 2:4 90 [;**00** 6.6 6.0 5.5 5.6 98 hl.L

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12.13 PIPE SUPPORT DESIGN

The preceding section has covered methods of providing flexibility in piping to limit stresses and reactions both to itself and to connections of sensitive equipment. This section is devoted to discussing methods of support for piping to limit stresses, reactions and deflections in piping and likewise protect connections to sensitive equipment.

12. 13. 1 Spacing of Supports

Although the normal spans utilized in pipeways are between 20 and 25 feet, occasionally there is a need for spacing supports to some abnormal span. Bechtel Standard L-518 provides a table showing maximum allowable pipe spans in pipeways for 2- through 24-inch nominal pipe size and for branch piping for 3/4-inch nominal diameter and larger. These spans were based on carbon steel piping at 450°F temperature. For other materials and higher temperatures special consideration should be given to determining allowable spans.

12.13.2 Ove hangs

In pipeways, the end span of a run of pipe requires special treatment. Permissible overhangs are shown in the charts of

SPACING OF PIPE SUPPORTS HANGERS

	MAXIMUM ALLOWABLE SPANS IN PIPEWAYS -\$ PI PE 2" 3" 4" 6" 8" 10" 12 14 16 18 20 24											
PI PE SIZE.	2"	3"	4	6 ^{II}	8	10	12	14	16	18	20"	24
DEFL.	.76	.G3	.77"	.84	.76	.80	.70	.67	.63	,60	3	.41

	MAX	KIMU	JM	AL	LOV	VAB	LE	SPA	NS]	FOR	BI	RAN	СН	LIN	ES*
SIZE	3 4	ı	11,"	2		4			10					••	
DEFL.	.29	.49	.74	I.Of	1.06	1.3	1.18	.75	.79	.64	.91	.74	.G2	.72	.38
FT.	10	13	17	20	25	30	35	35	40	40	45	45	45	50	50

- ♦ Normal spans for general pipeway design shall be within 20¹ to 25,
- * Lines from pipeway to other lines and/or equipment,

NOTES

- 1. Calculations of pipe spans are based on:
 - a) 3/4" through 1½" Pipes, Wal I Thickness Sch. 80
 2" through 6 11 Pipes, Wal 1 Thickness Sch. 40
 8" through 12" Pipes, Wal 1 Thickness Sch. 30
 14'' through 24" Pipes, Wal 1 Thickness Sch. 20
 - b) Pipes filled with water and insulated for 450°F.

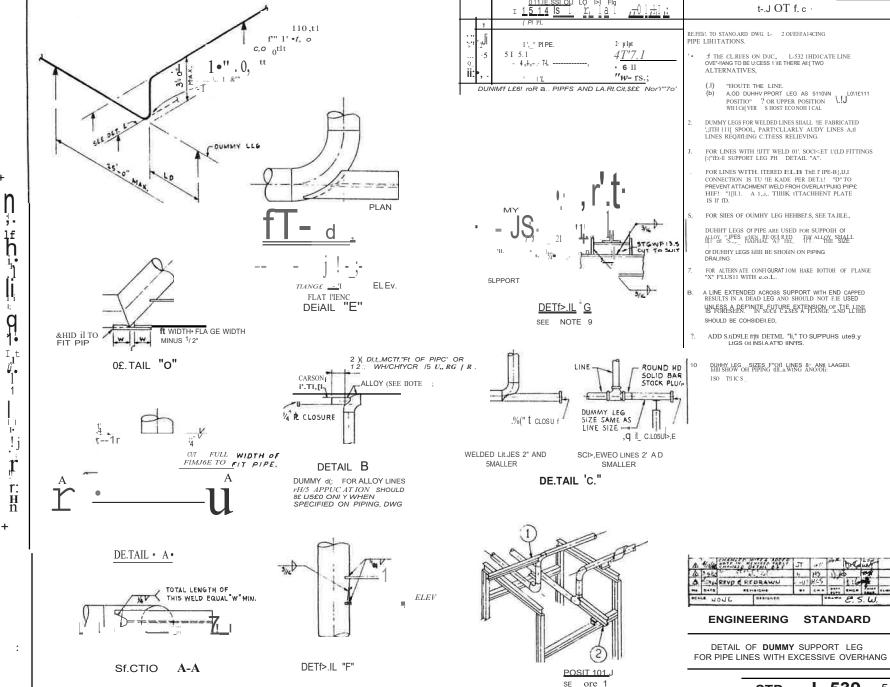
Spans in the tables above are limited by longitudinal bending stress of 9000 PSI and by acceptable pipe deflection between supports determined from past experience.

2. Supporting of the end span of a continuous run of pipe in the main pipeway shall be given special consideration ullet

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No.	DATE		IIEVISIONS	IY	CH'K '	APPII
		111	BECHTEL ENGINEERING STANDARD	JOI No. !::, T	AN I) A	RD
	- (- /		TABLE OF ALLOWABLE PIPE SPANS FOR	SP[Ci DE	S. GUIDE No.	REV
10/10)/68	100	PIPEWAYS AND FOR BRANCH LINES	L-5	518	2
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Bechtel Standard L- 32. Where the overhang is excessive, either dummy legs must be added or additional beams or other manner of support must be employed. Refer to Standard L-539 for Dummy Support Attachments.

12. 13. 3 Restraints (Guides, Anchors, and Stops)

A restraint may be defined as a device which prevents, limits, or resists the thermal displacement of piping. Of course, all supports upon which the pipe rests tend to restrain movement in at least onedirection, but let us disregard this idea while discussing guides, stops, and anchos.

The use of restraints may be required for the following reasons:

- To protect sensitive equipment
- To control pipe movements
- To maintain axial alignment
- To ensure cor ect function of expans ion loops
- To avoid overstrain of reduced line sections
- To isolate mechanical vibration

- To prevent disengagement of flexible couplings
- To ensure predictability of the system

There are several other cases wherer estraintsnlay be used.

The previous instances are the most common ones. Specific types of restraints are used in the following ways.

Guides: A long length of pipe under direct axial compression constitutes a weak column subject to buckling. The ability of the pipe to move axially against elastic and frictional resistance is impaired, and a state of stress capable of buckling the pipe is mo e readily achieved,

To prevent this condition, we must inc-orporate some form of lateral restraint, such as a guide, along the line length. We must take care, however, to ensure that guides are not placed near areas of directional change or areas where flexibility is necessary.

Anchors: Anchors as generally understood are rigid devices which maintain points of full fixation preventing any rotation and translation at the point. Seldom is this type of anchor used, therefore the term anchor has been used to indicate an "axial" stop.

This device prevents translatory movement in the axial direction, but normally pe mits rotation of the pipe. Anchors are used primarily to protect equipment from reaction overload and to limit movement.

An anchor, in most cases, also acts as a support. Refer to Bechtel Standard Drawing M-624 for Anchor and Guide Details.

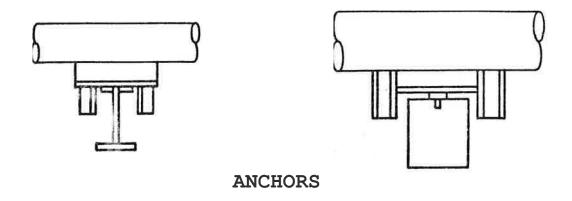


Figure 12-18

12.13.4 Frictional Forces

A pipe subject to thermal movement will produce a horizontal force on supporting members due to frictional resistance.

This force is independent of line temperature and is little affected by the amount of movement taking place.

The sum of the forces exerted by the pipe upon var in a supporting members will react at the line anchor. We should therefore space loops and anchors in long runs of pipe so that there are approximately equal amounts of pipe on each side of an anchor. In this way, we can balance frictional forces and make anchor loads more reasonable.

We can also employ various types- of contact faces (Figure 12-19) in supporting the system which will reduce frictional for ces.

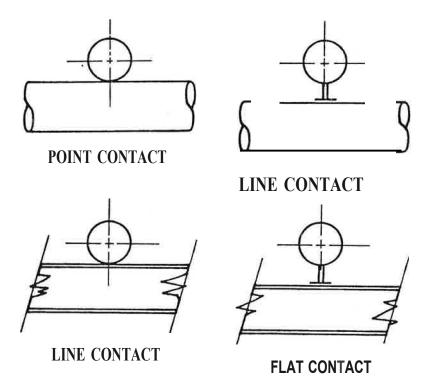


Figure 12-19. Types of Contact F aces.

The friction coefficient can vary from O. 1 to O. 75, depending upon surface conditions; but it is normally from O. 2 to 0. 3, or a little higher if the line is guided.

Rollers, self-lubricating bearing plates, and Teflon plates may be used to reduce frictional forces *if* the support members, equipment, or anchors will otherwise be over-loaded.

12. 13. 5 <u>Lines from Vertical Vessels</u>

Lines hanging from vertical vessels are usually supperted close to the vessel nozzles for at least tworeasons:

- To minimize differential expansion
- To allow disengagement of piping with support still provided

Apply the following rules when routing lines adjacent to vertical vessels:

The distance from the pipe to the vessel shell varies according to Bechtel Engineering Standard Drawings M-600, Notes 1 & 2. The designer should attempt to keep the piping as close to the vessel shell as possible. This proximity reduces the moment acting upon the vessel shell at support and guide locations.

Lines must be guided at certain intervals to prevent vibration or sway from wind. The extent of this provision depends upon the pipe size. Bechtel Standards regarding guide spacing must be used where possible. For application and details refer to Standard Drawings M-600, M-601 and M-602. For Minimum Spacing of Lines Located radially on Vertical Vessels, see Std. Dwg. M-612.

12, 13, 6 Stress Relieved Vessels

All piping systems related to stress-relieved vessels must be given special priority. The pressure vessel job supervisor will provide a list of stress-relieved vessels with required due dates established by the vessel fabricator for stress relief work. These dates will be marked on tags placed on vessel models.

All design work must be completed six (6) weeks prior to these critical dates. The stress department will review and approve work. The pipe support group will complete detailing and issue all vessel attachments to the vessel fabricator four (4) weeks prior to the actual stress relief work.

Field welding is not permitted on stress-relieved vessels. No changes to pipe routing are allowed after the expiration of these

dates; if there are unavoidable design changes, the revision must be coordinated with the stress depa tment and vessel fabricator immediately to avoid serious problems, additional back charges, or delays in delivery.

The procedure for defining and locating vessel attachments required on stress-relieved vessels is shown on Bechtel Standard Drawing M-610. See Figure 12-20 for a typical pipe support detail sent to vessel fabricators.

12. 13. 7 <u>Miscellaneous Design Guides</u>

The following miscellaneous Pipe Support Design Guides are attached to Section 12 for your information.

- (1) Supports for Utility Lines from Vessels andPlatforms M-603
- (2) Supports for Heater Piping M-607
- (3) Supports for Guides for Vertical Lines M-608
- (4) Typical Hanger Supports M-609
- (5) Supports for Control Valve Manifolds M-611
- (6) Typical Isometric Pipe Support Mark-Up M-613

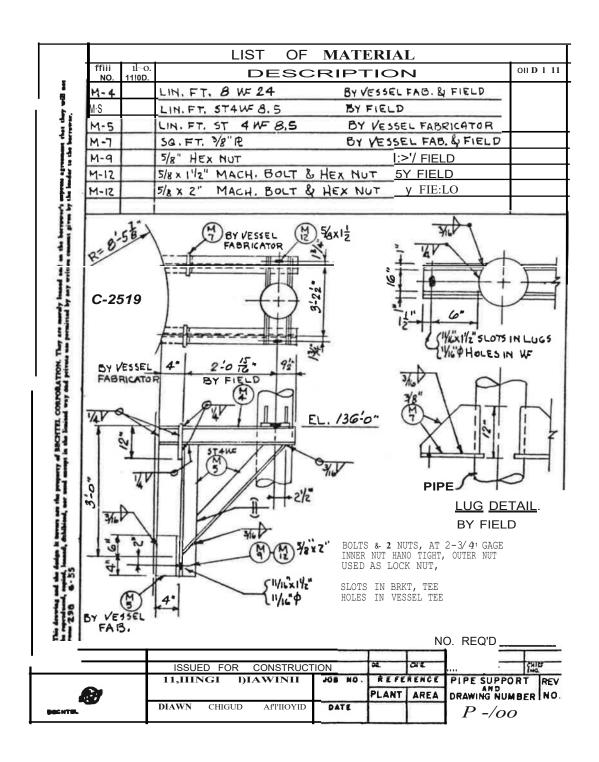
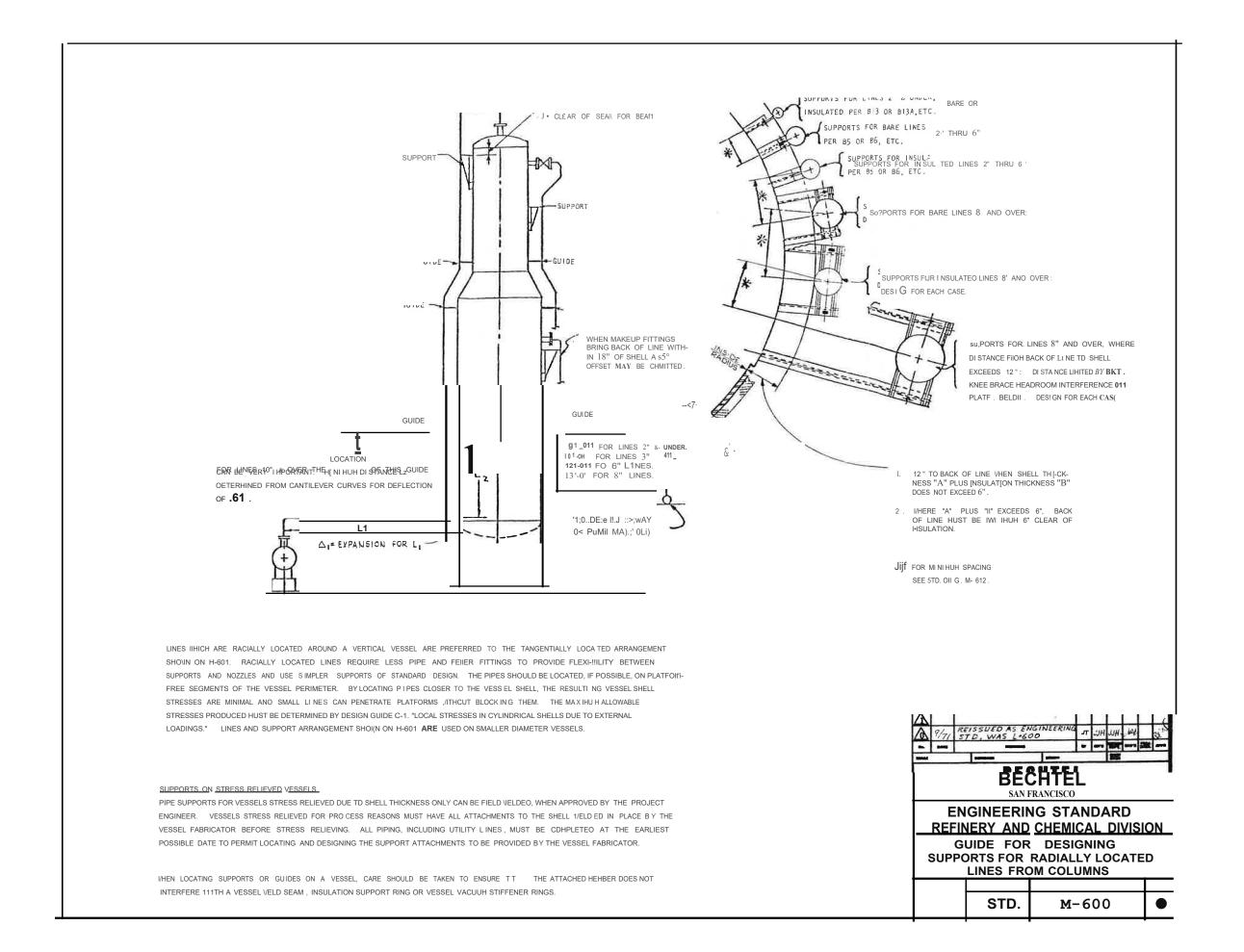
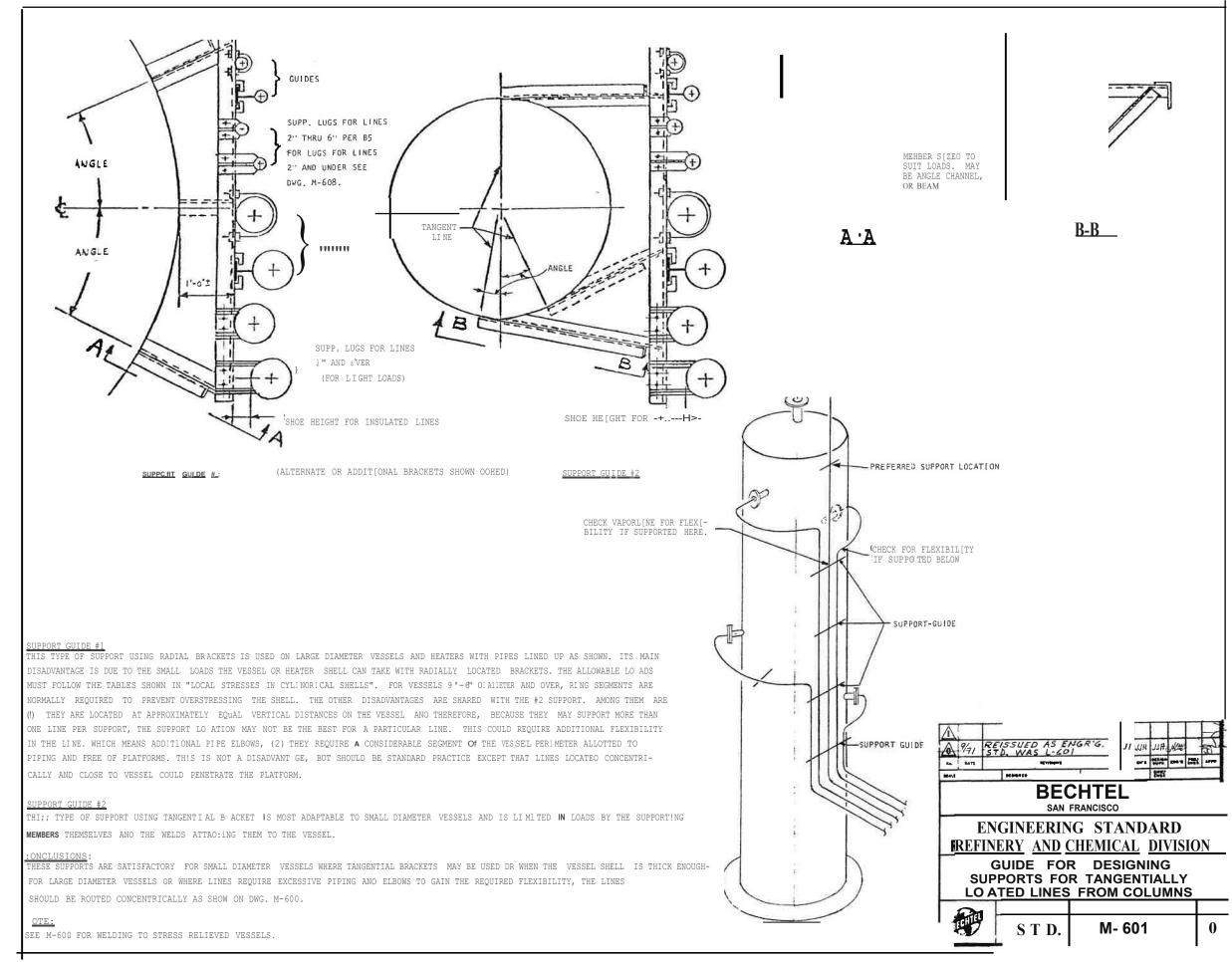
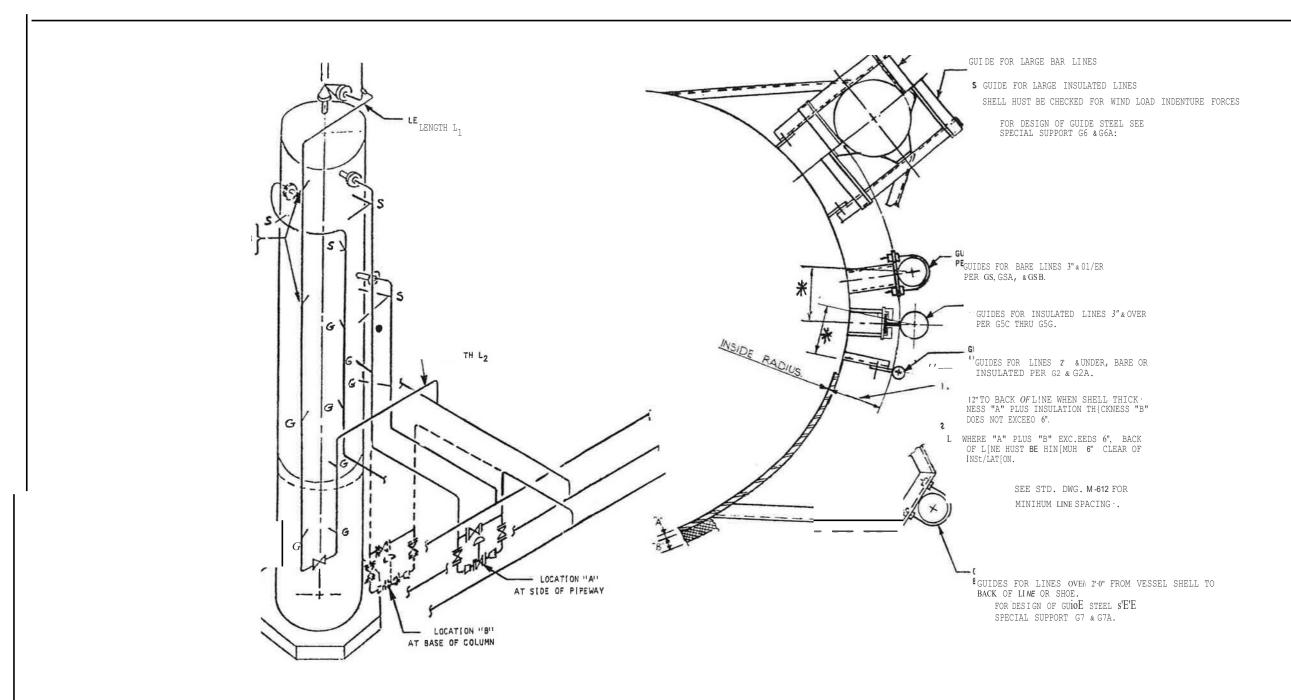


Figure 12-20.







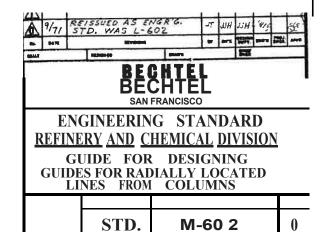
GUIDES SHOWN ARE TYPICAL FOR RADIALLY LOCATED LINES, STANDARD VERTICAL SPACINGS ARE SHOWN IN TABLE ON THE STANDARD GUIDE DETAILS EXCEPT FOR THE LOCATION OF THE BOTTOM GUIDE WHICH IS SHOWN ON DRAWING M-600,

THE LOCATION 0 THE SUPPORT FOR A RELIEF PURGE LINE IS ALMOST ALWAYS CRITICAL FOR THE FOLLOWING REASONS:

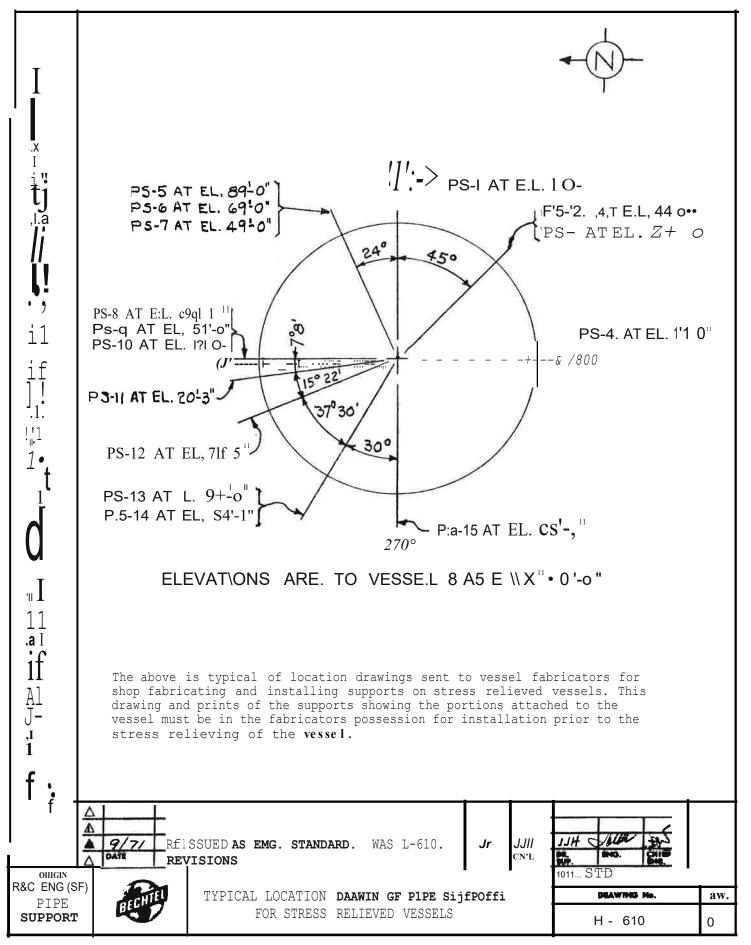
- (I) THE RISER FROM THE VALVE NEAR GRADE IS USUALLY AT AL\61 ENT TEMPERATURE WHICH MEANS BELOW FREEZING IN SOME PLACES IN THE WINTER BECAUSE THE PURGING OPERATION IS NOT FREQUENT.
- (2) THE VESSEL HELL 1'IAY BE HOT OVER MOST OF ITS LENGTH RESULTING IN CONSIDERABLE EXPANSION FROM SKIRT TO CONNECTION TO THE

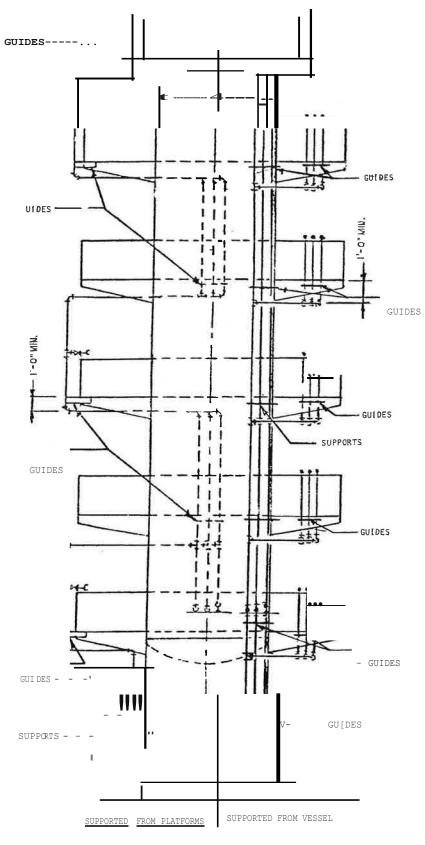
THE LOCATION OF THE SUPPORT THEN MUST SE SELEC'RE:D SO THAT ENGTH L1 WILL.TAILE THE VESSEL GROI, TH ABOVE THE SUPPORT AND LENGTH L2 WILL TAKE THE VESSEL GROWTH BELOW THE SUPPORT. IF NO LOCATION CAN SE FOU D, EITHER OR BOTH LENGTH L1 NO Lz MUST SE . I NCREASED TO SUIT OR AN EXPANSION LOOP PROVI EO.

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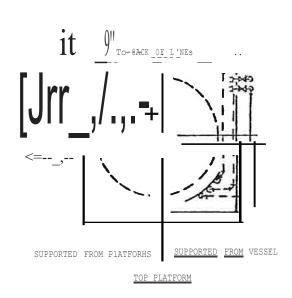


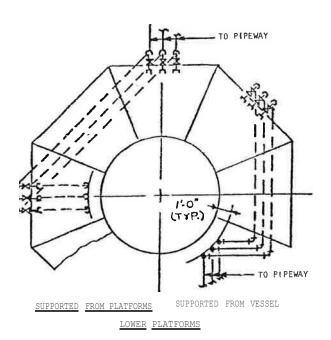
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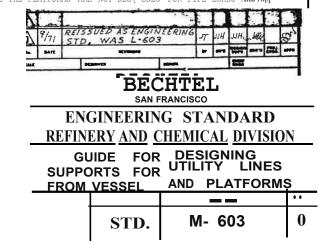


SUPPORTING AND GUIDING L[NES FROM vEss:

T IS METHOD [S PREFERRED BECAUSE THE SUPPORTS CAN BE LOCATED ON THE VESSEL WHICH [S CAPABLE OO TAKING THE SUPPORT LOADS AND BY SUPPORT [G ABOUT THE MID POINT OF T E VESSEL, THE BRANCHES TO THE PLATFORM O RI/NS TO THE PIPEWAY ONLY HAVE TO BE FLEXIBLE ENOUGH FOR HALF THE TOTAL VESSEL GROIIT4. THE L[NES ARE GUIDED ABOVE AND BELOW THE SUPPORT AT STANDARD INTERVALS. TO GIVE RIGIDITY TO THE 1405E CONNECTIONS THE FIELD FASTENS EACH HOSE CONNECTION TO THE PLATFORM HAND RAIL. BECAIJ E OF THIS, SU[DES ONLY SHOULD BE PROVIDED FOR TIE RISERS FROM THE UNDERSIDE OF THE PLATFORMS. UTILITY UNES BEING SMALLAT J LOCATED CLOSE TO SHELL CAN PENETRATE PLATFORMS WITHOUT BLOCKING THEM.

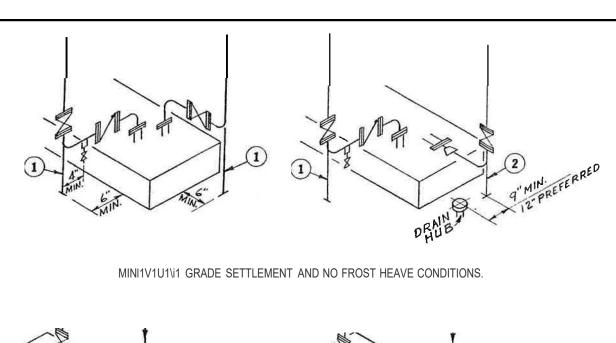
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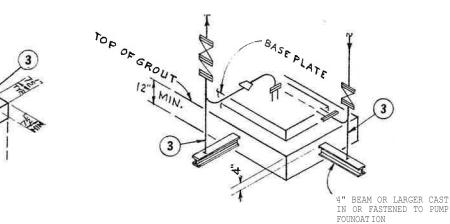
PUMP FOUNDATION EXTENSIONS

INTEGRALLY CAST WITH FOUNDATION

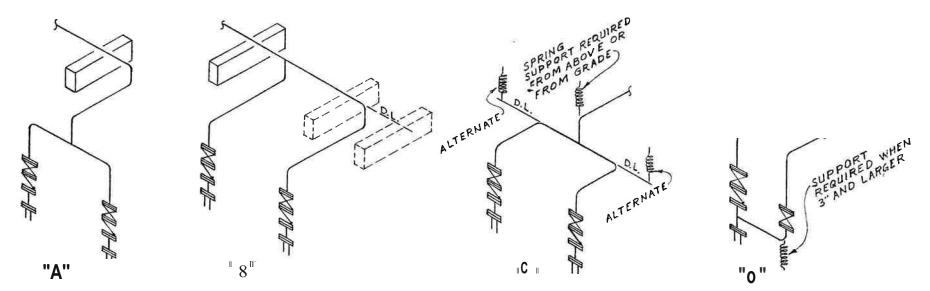


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PUMP FOUNDATION EXTENSIONS INTEGRALLY CAST WITH FOUNDATION



FROST HEAVE OR GRADE SETTLEMENT CONDITIONS.



I/HEN THE LINES ARE RUN VERTICALLY FROM TOP SUCTIONS OR TOP DISCHARGES (SEE A, B, CANO D), THE PUMPS MUST BE CAPABLE OF SUPPORTING THE VERTICAL LOADS IMPOSED. PIPING ARRANGEMENTS "A" AND "B" IMPOSE VERTICAL LOADS ONLY ON PUMPS,

PIP ING ARRANGEMENTS "C" AND "D" PLACE ECCENTRIC LOADS ON THE PUMP NOZZLES INDUCING MOMENTS WHICH CAN CAUSE EXCESSIVE PUMP WEAR AND MAINTENANCE OR PUMP DRIVER MISALIGNMENT UNLESS THE MOMENTS ARE REMOVED WITH ADDITIONAL SUPPORTS,

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6" AND LARGER	ADJUSTABLE OR SPRING	ADJUSTABLE OR SPRING	ADJUSTABt E

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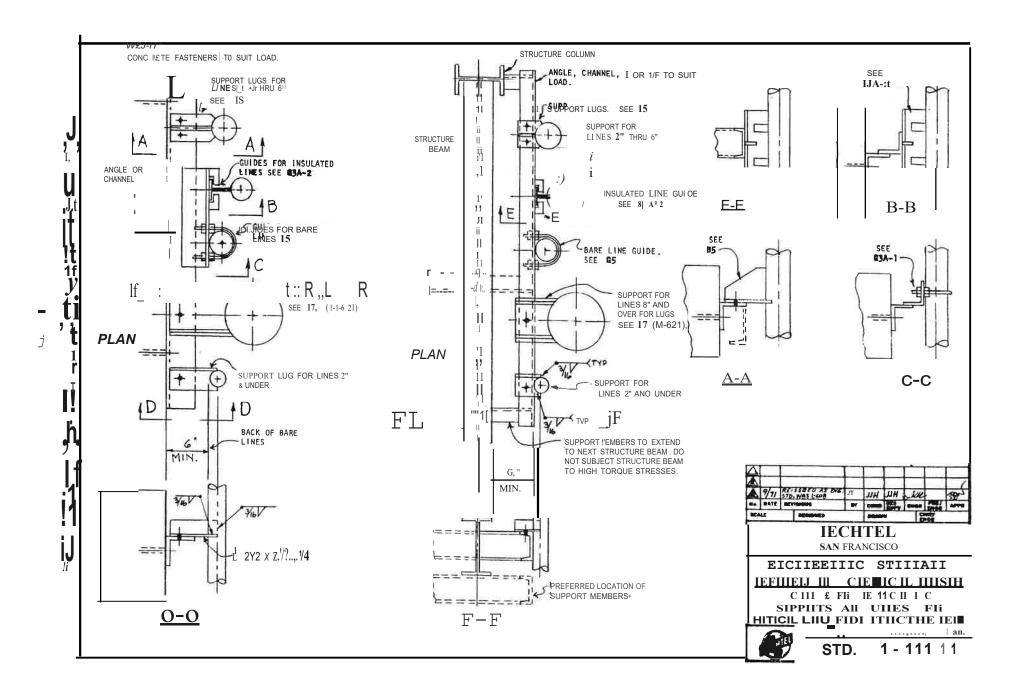
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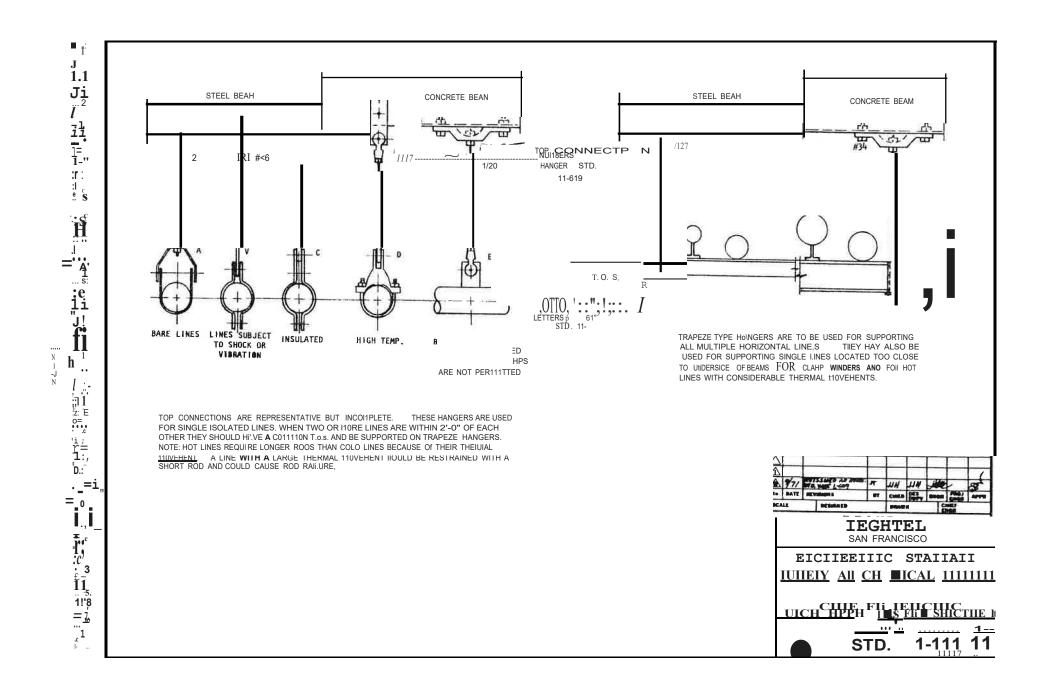
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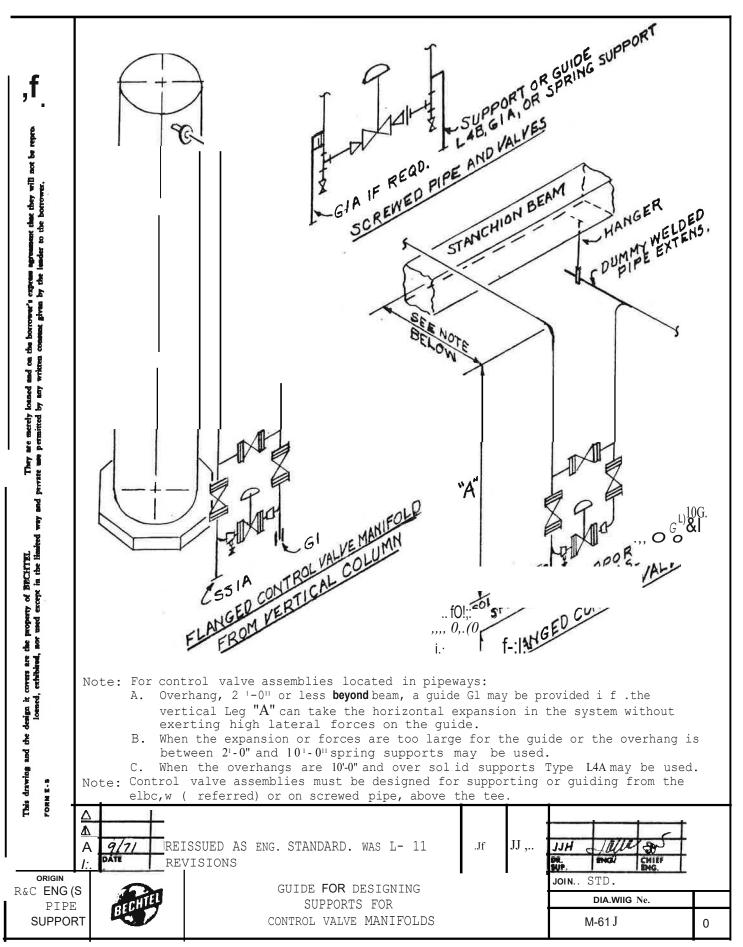
ENGINEERING STANDARD REFINERY AND CHEMICAL DIVISION

GUIDE FOR DESIGNING SUPPORTS FOR PUMP PIPING

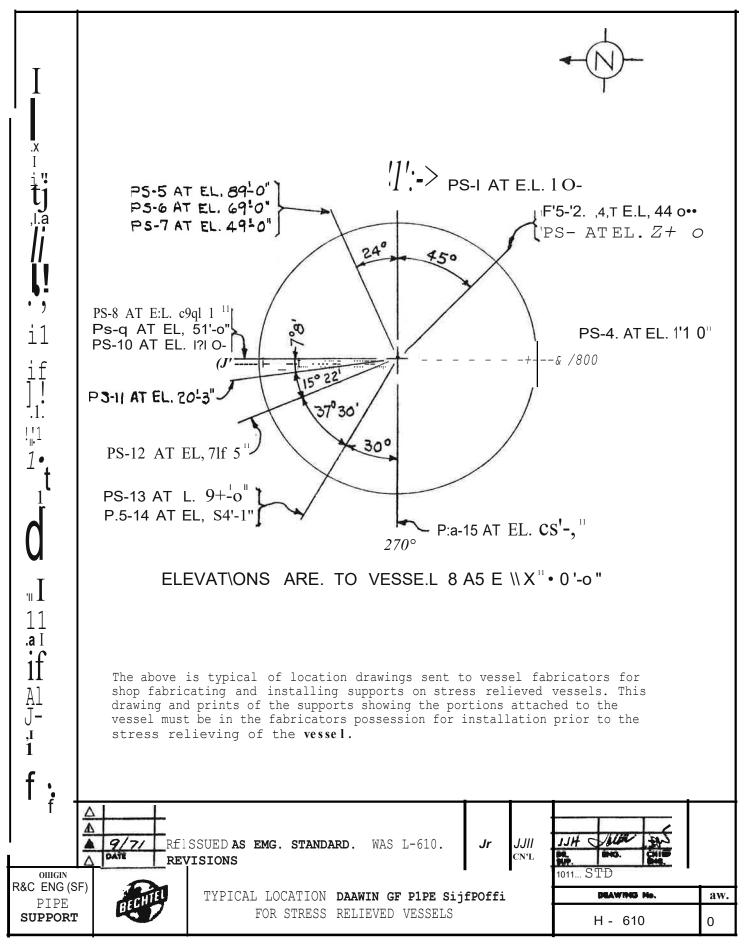
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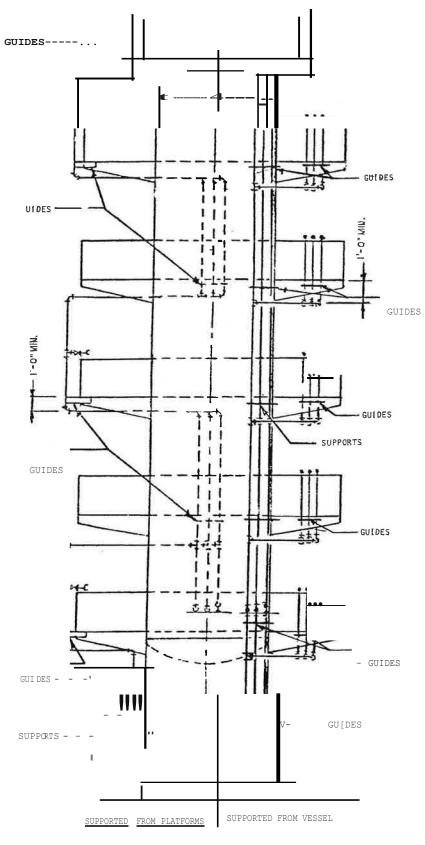




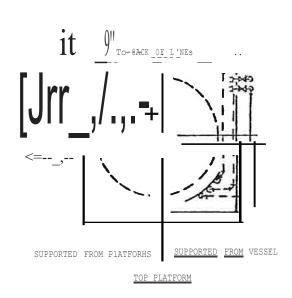


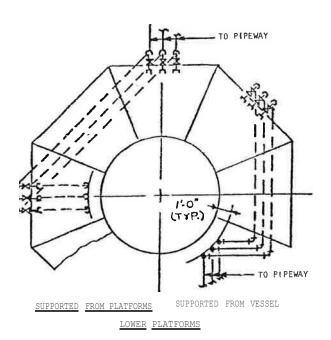
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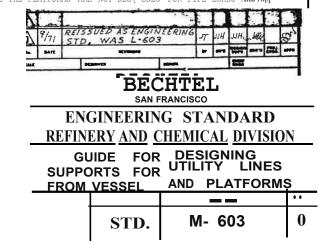


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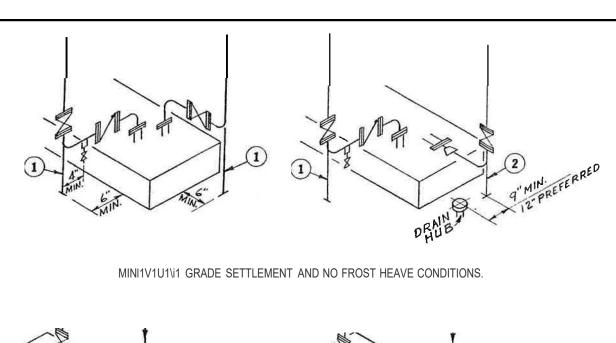
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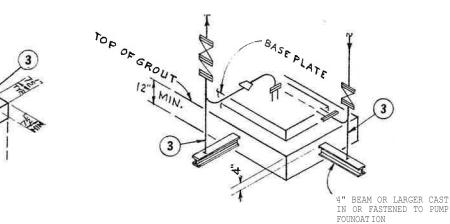
PUMP FOUNDATION EXTENSIONS

INTEGRALLY CAST WITH FOUNDATION

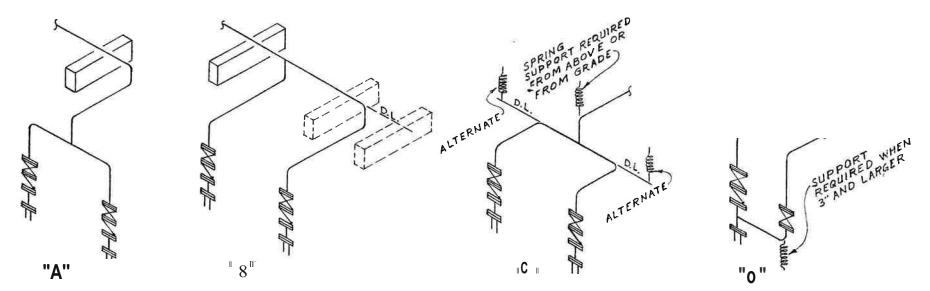


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PUMP FOUNDATION EXTENSIONS INTEGRALLY CAST WITH FOUNDATION



FROST HEAVE OR GRADE SETTLEMENT CONDITIONS.



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PIP ING ARRANGEMENTS "C" AND "D" PLACE ECCENTRIC LOADS ON THE PUMP NOZZLES INDUCING MOMENTS WHICH CAN CAUSE EXCESSIVE PUMP WEAR AND MAINTENANCE OR PUMP DRIVER MISALIGNMENT UNLESS THE MOMENTS ARE REMOVED WITH ADDITIONAL SUPPORTS,

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4" AND SMALLER	L4A OR L4H	L4A OR L4H	L4A OR L4H
6" AND LARGER	ADJUSTABLE OR SPRING	ADJUSTABLE OR SPRING	ADJUSTABt E

SUCTIOLJ ANO DISCHARGE PIPING, 4" AND SMALLER, MAY BE SUPPORTED BY A SOL ID BASE SUPPORT, LINES 6" AND LARGER SHOULD BE SUPPORTED BY **AN** ADJUSTABLE SUPPORT OR, IN SOME CASES, BY A SPRING SUPPORT,

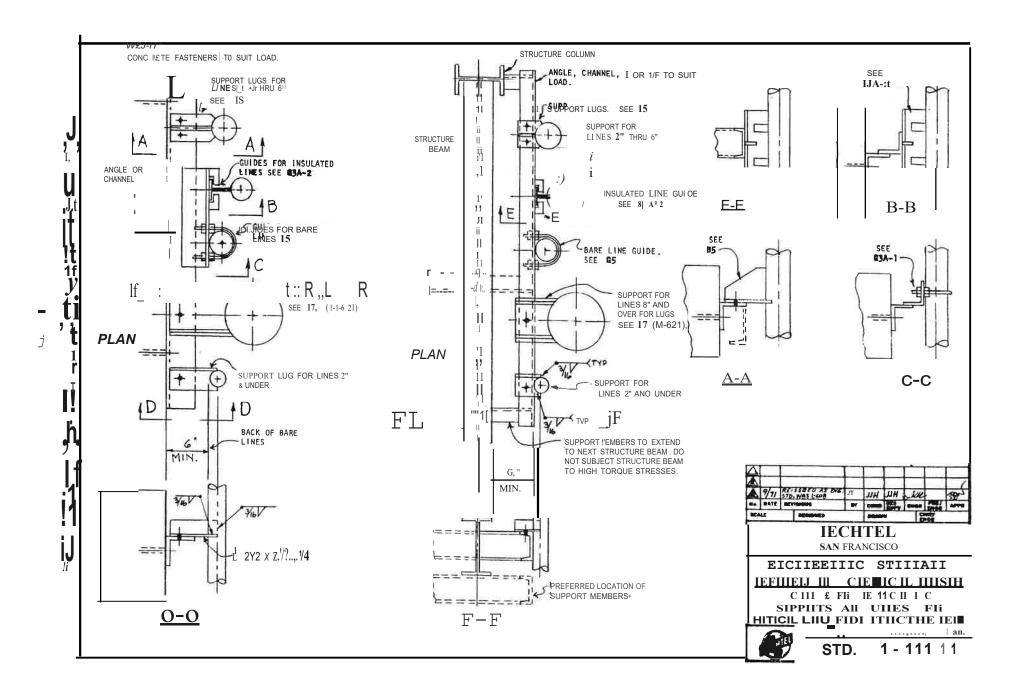
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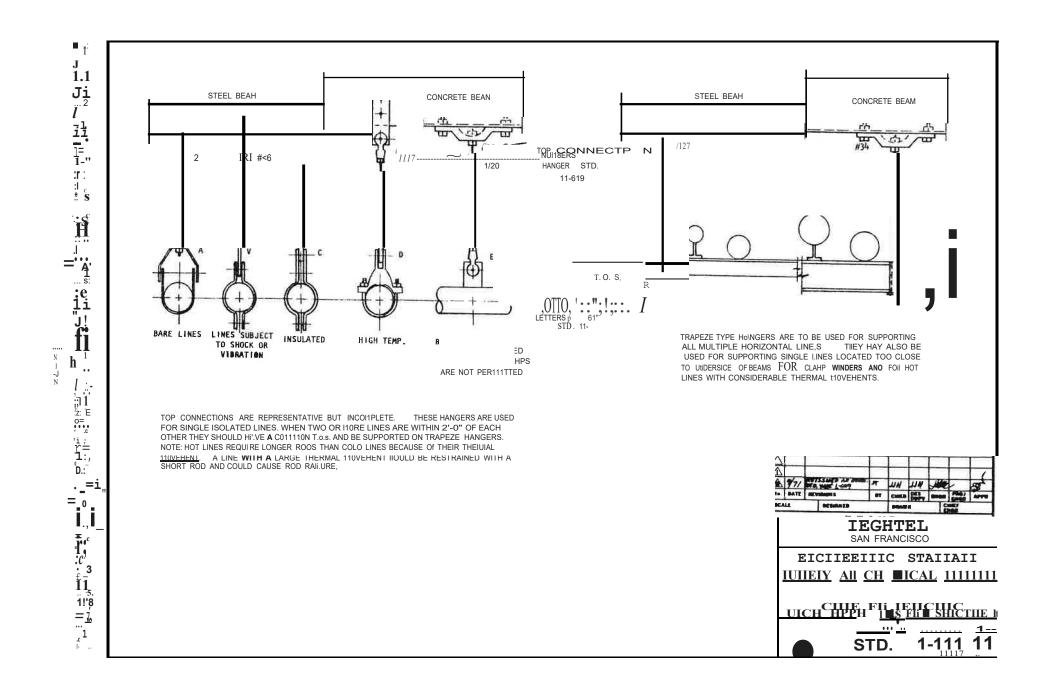
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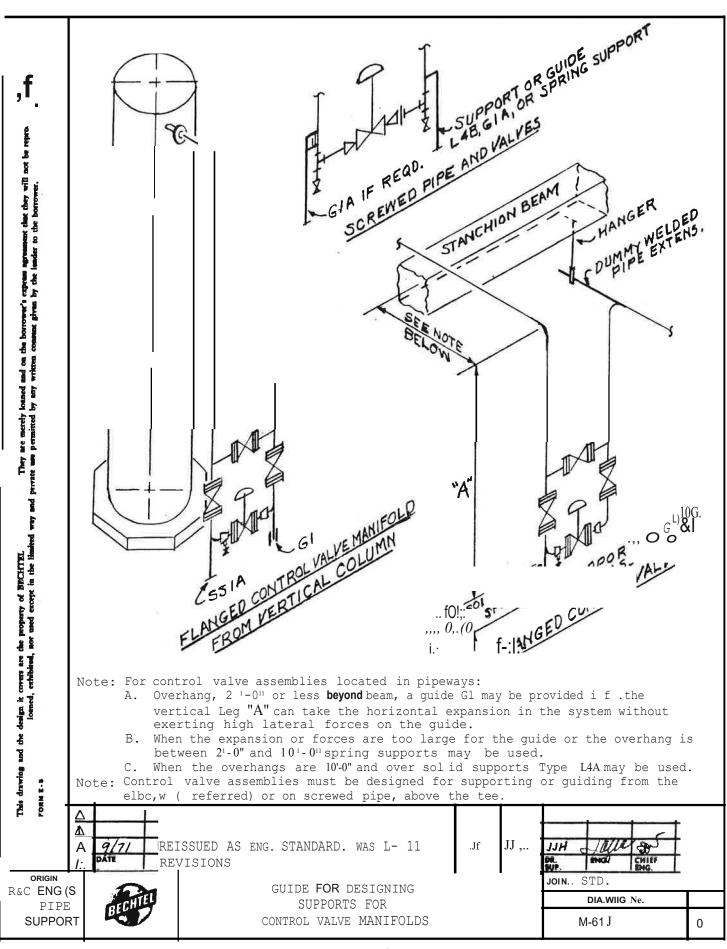
ENGINEERING STANDARD REFINERY AND CHEMICAL DIVISION

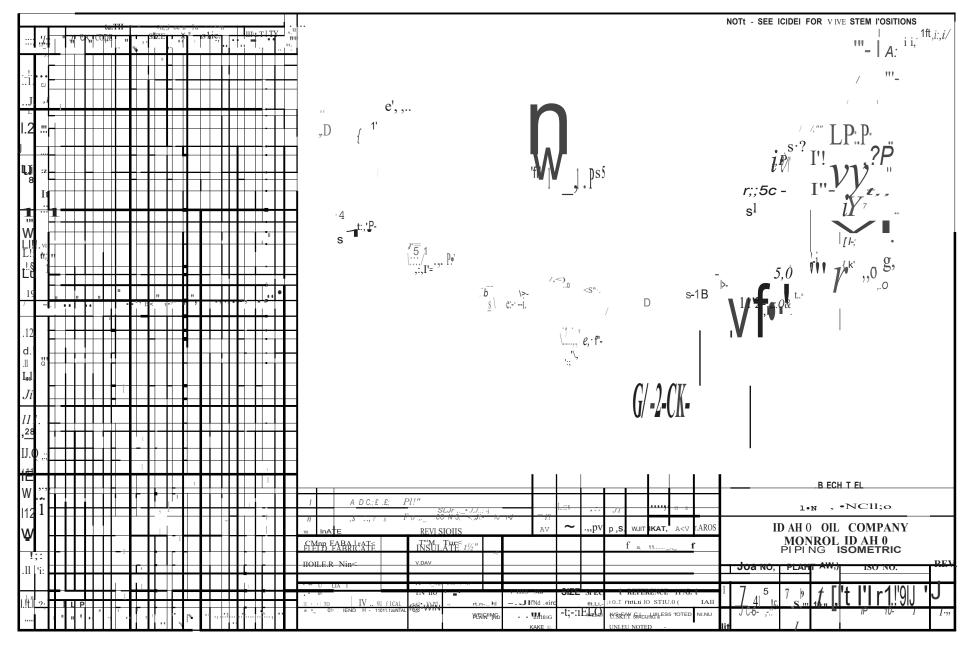
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ONE OF THE FOLLOWING PLPE SUPPORT STAMPS IS PLACED ON THE PIPING ISOMETRIC WHEN CONVENIENT:

NO PIPE SUPPORTS REQUIRED
THIS INDICATESTHATTHE PIPE IS SELFSUPPORTING OR THAT THE EXISTING SUPPORTS
ARE SUFFICIENT.

FIELD TO SUPPORT

SUPPORTS ARE REQUIRED AND LINES ARE SUPPORTED BY THE FIELD USING STANDARD DRAWING M-628 AS A GUIDE.

PIPE SUPPORTS BY FIELD

THIS STAMP IS INTENDED FOR ISO METRICS WHERE PIPE FABRI CATOR USUALLY SUPPLIES WELDID ATTACHMENTS BUT DU£ TO SCHEDULE ETC., FIELD WILL FABRI CATE COMPLETE P.S. AND ATTACH.

PIPE SUPPORTS ATTACHED BY FIELD

THIS STAMP IS PUT ON PIPING ISOMETRICS WHERE STANDARD DRAWINGS AND SPECIFICATIONS DICTATE SHOP TO ATTACH BUT DUE TO SCHEDULE OR PROCUREMENT CONVENIENCE, FIELD IS INSTRUCTED TO RECEIVE FABRICATED P. S. AND ATTACH TO PIPE.

NO \','E:.:: , :=:: SU?PORT ATTACH:;;::-<=- , P.:C:QUIRED BY PIPE FAGI'<ICATOR

THIS STAMP IS INTENDED FOR ALLOY PIPES AND STRESS RELIEVED. PIPES. PIPE SUPPORTS ARE REQUIRED BUT FIELD WILL SUPPLY AND ATTACH, E.G., CLAMPED SHOES, BRACKETS OR GUIDES. PIPE SUPPORT ATTACHMENT FABRICATED REQUIRED FOR ______ONLY

THIS STAMP DIRECTS PIPE FABRICATOR TO MAKE AND ATTACH CERTAIN PIPE SUPPORTS ONLY. REMAINING PIPE SUPPORTS SHOWN ON THE ISOMETRIC WILL BE MADE AND ATTACHED BY THE FIELD.

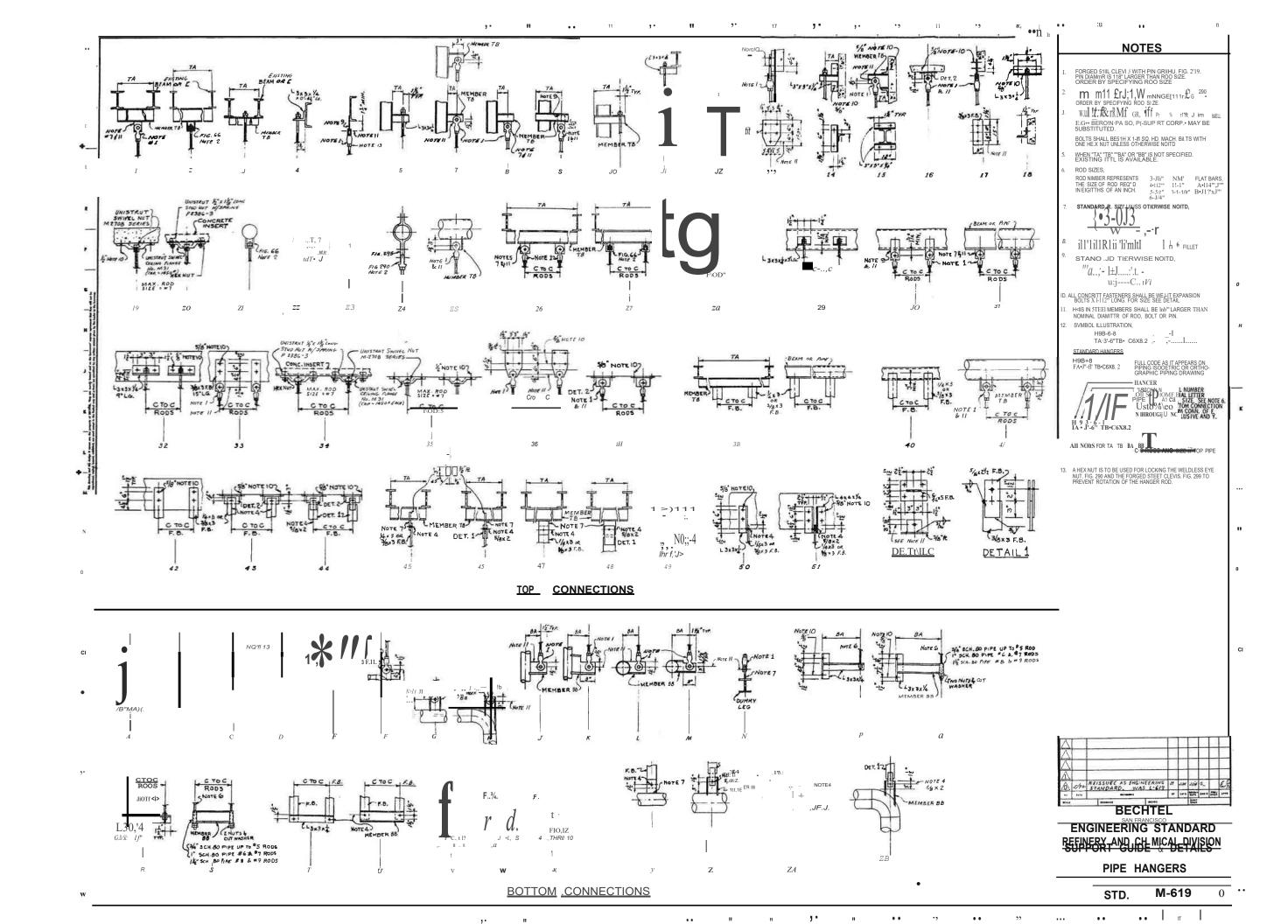
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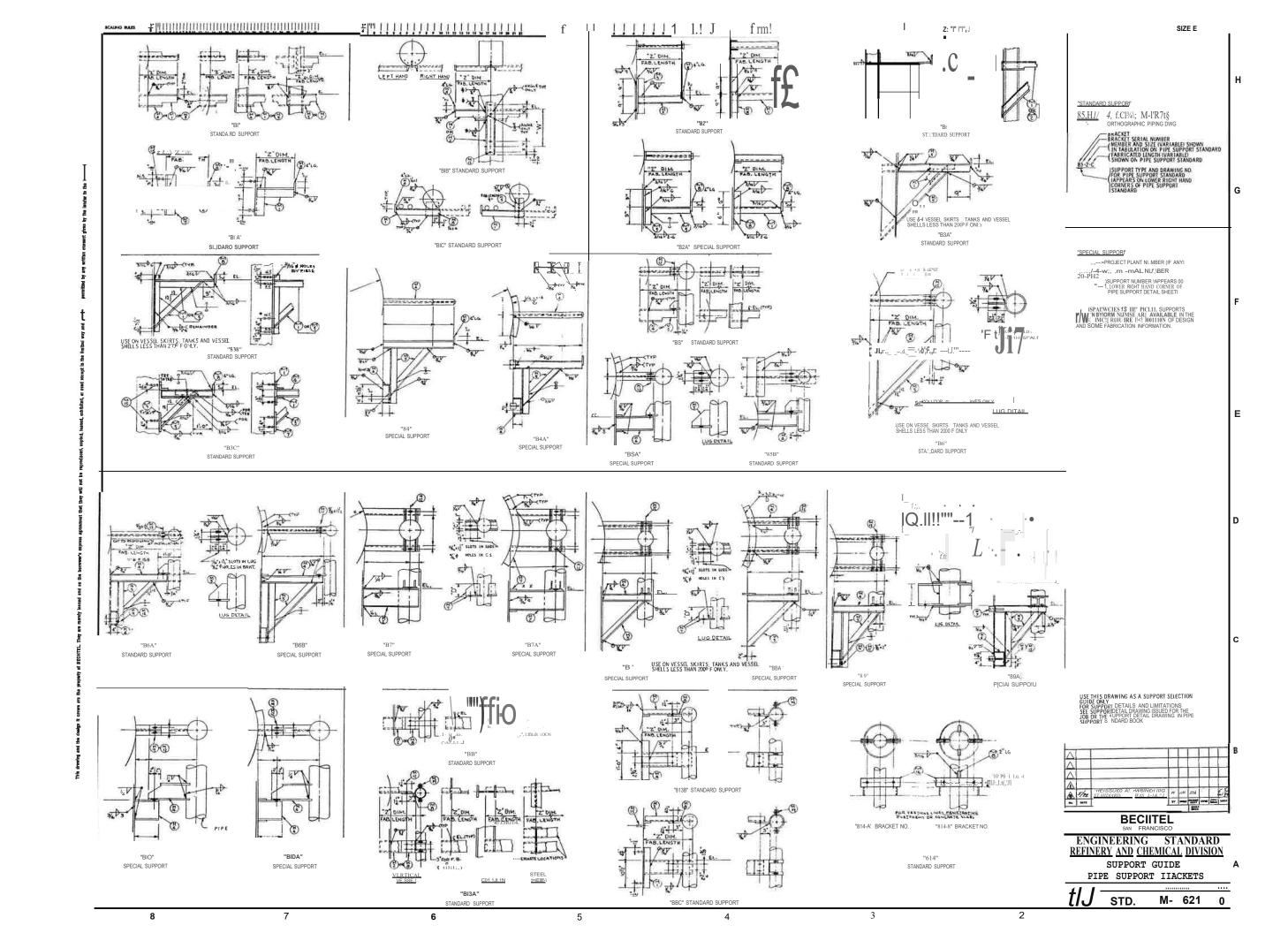
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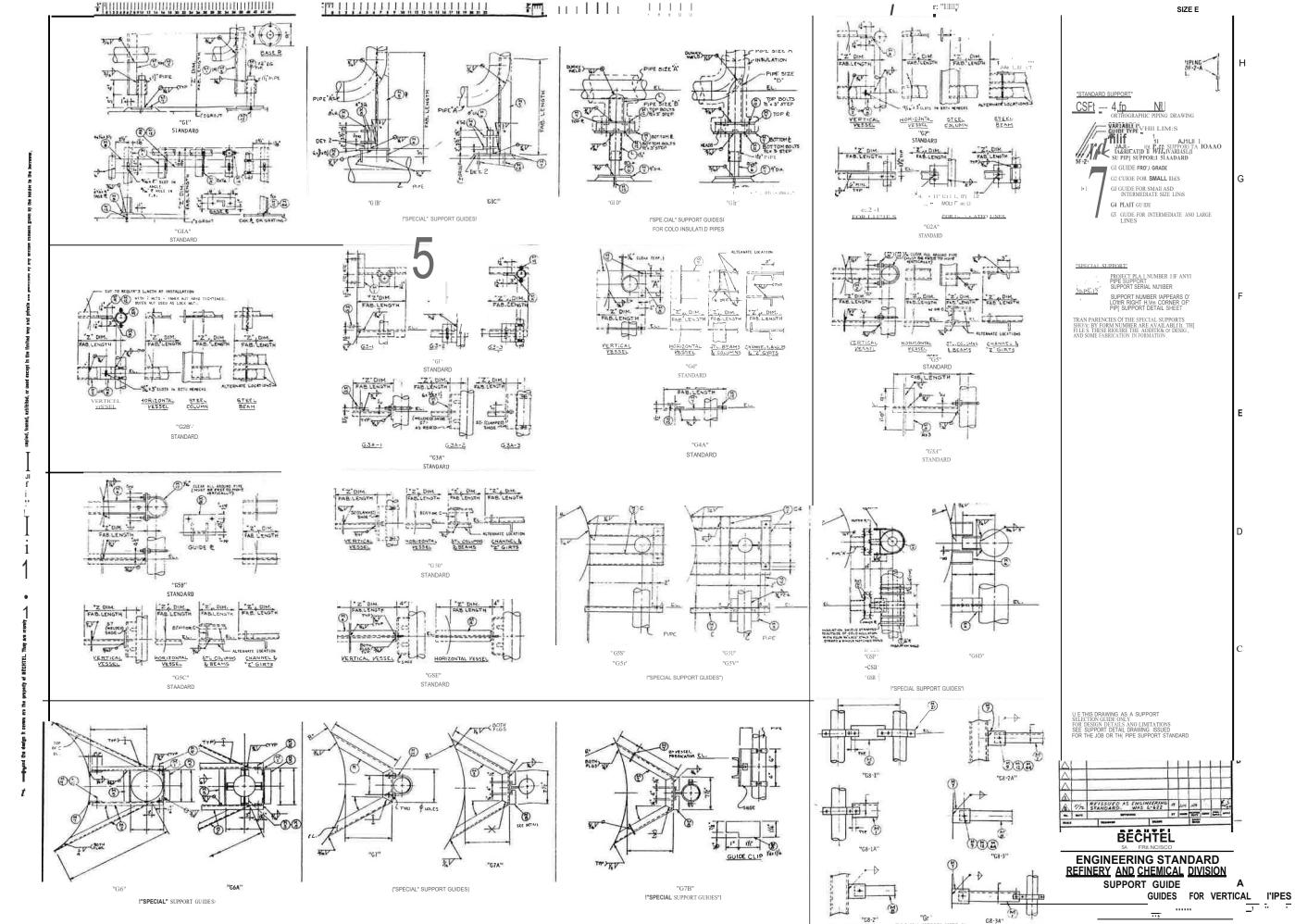
ENGINEERING STANDARD REFINERY AND CHEMICAL DIVISION

TYPICAL MARKED-UP PIPING ISOMETRIC

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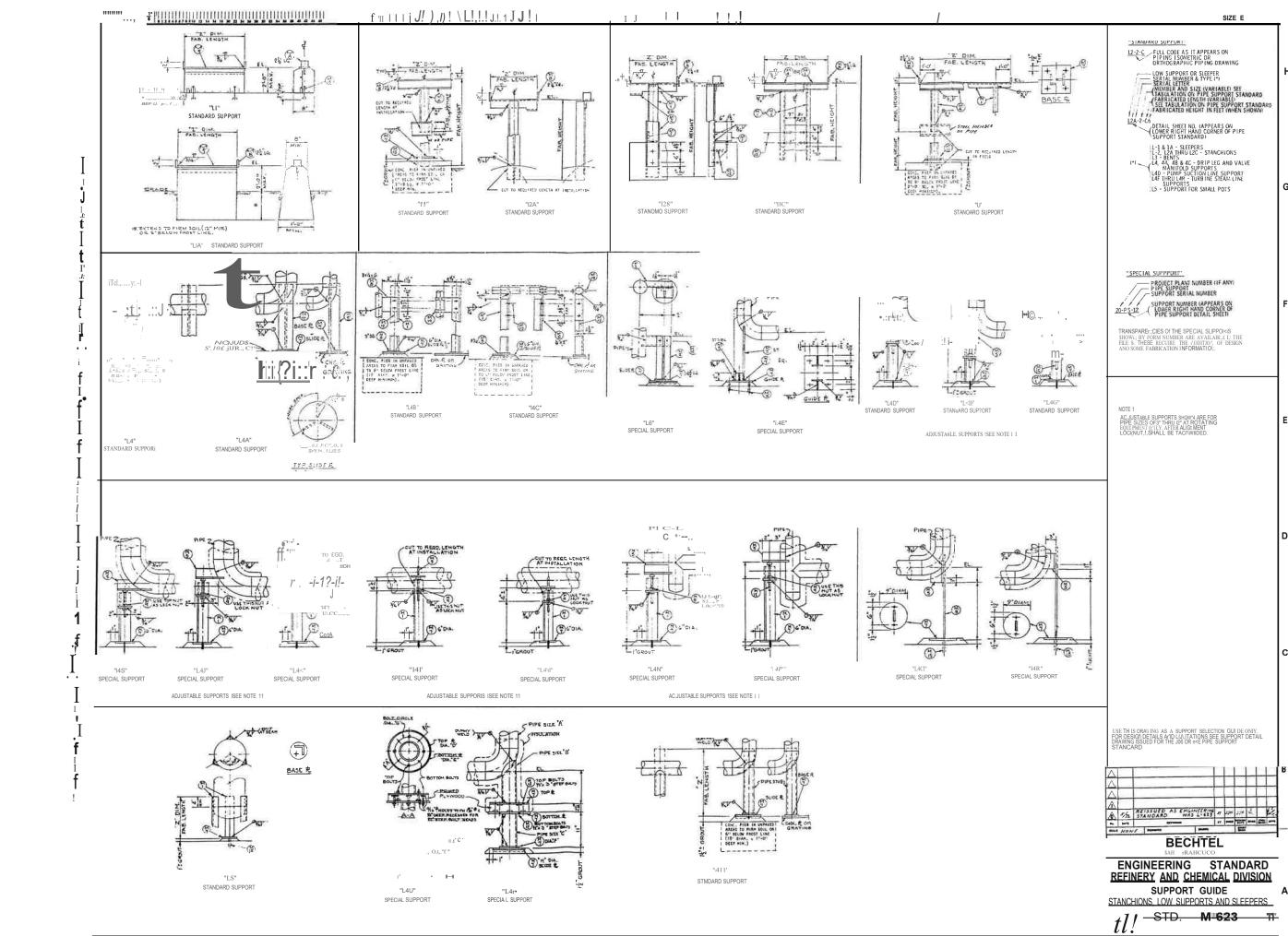


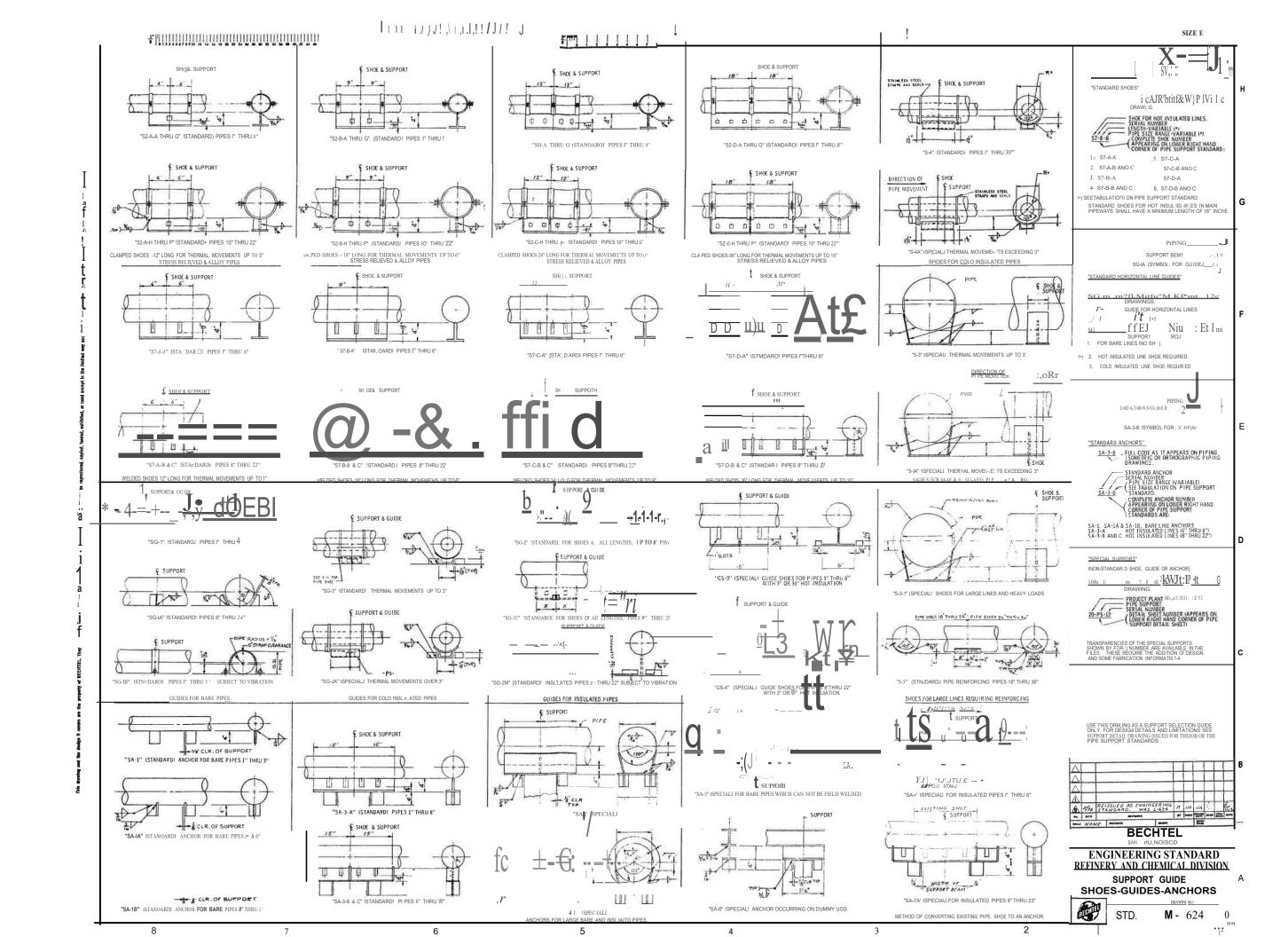


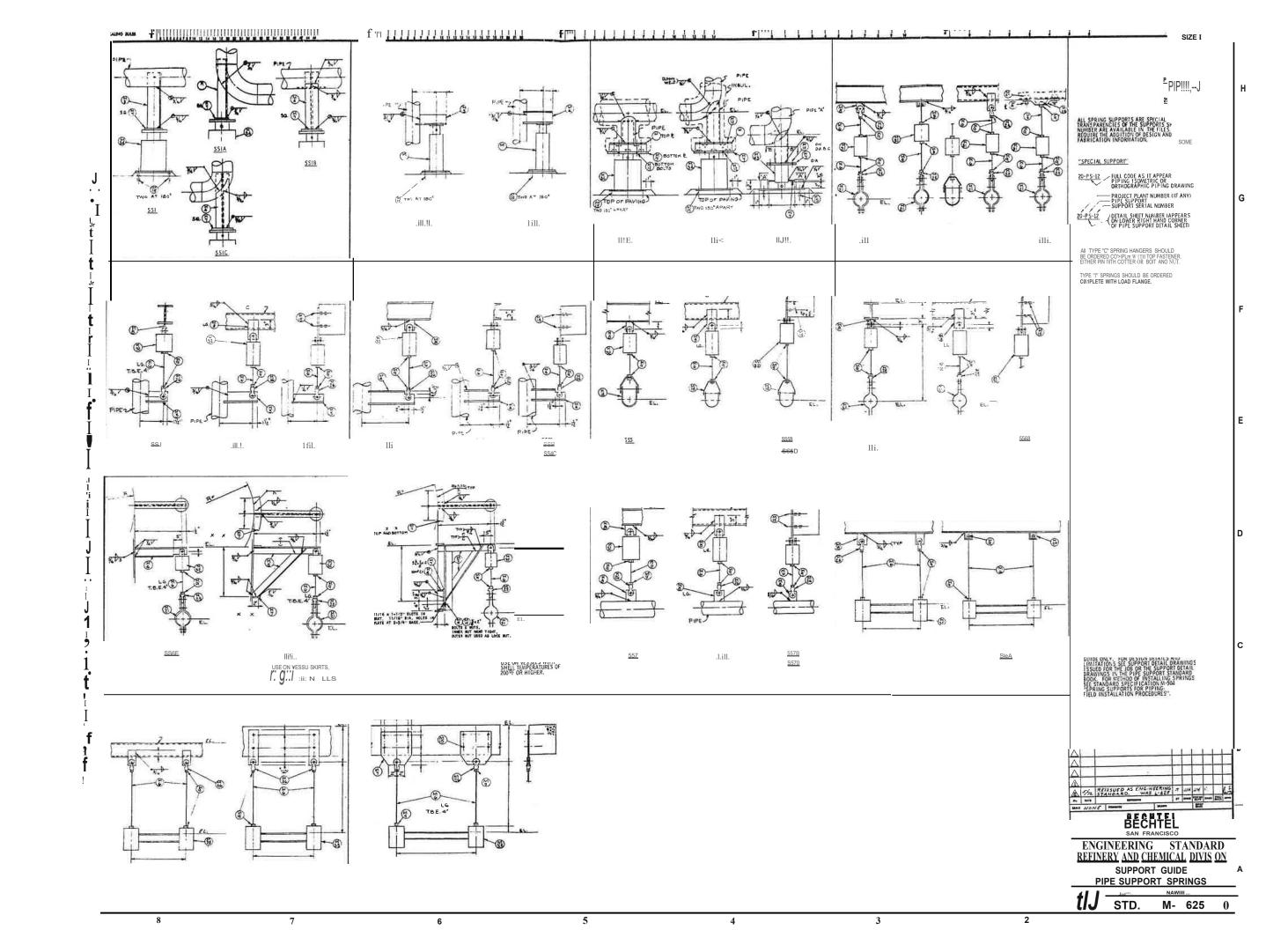


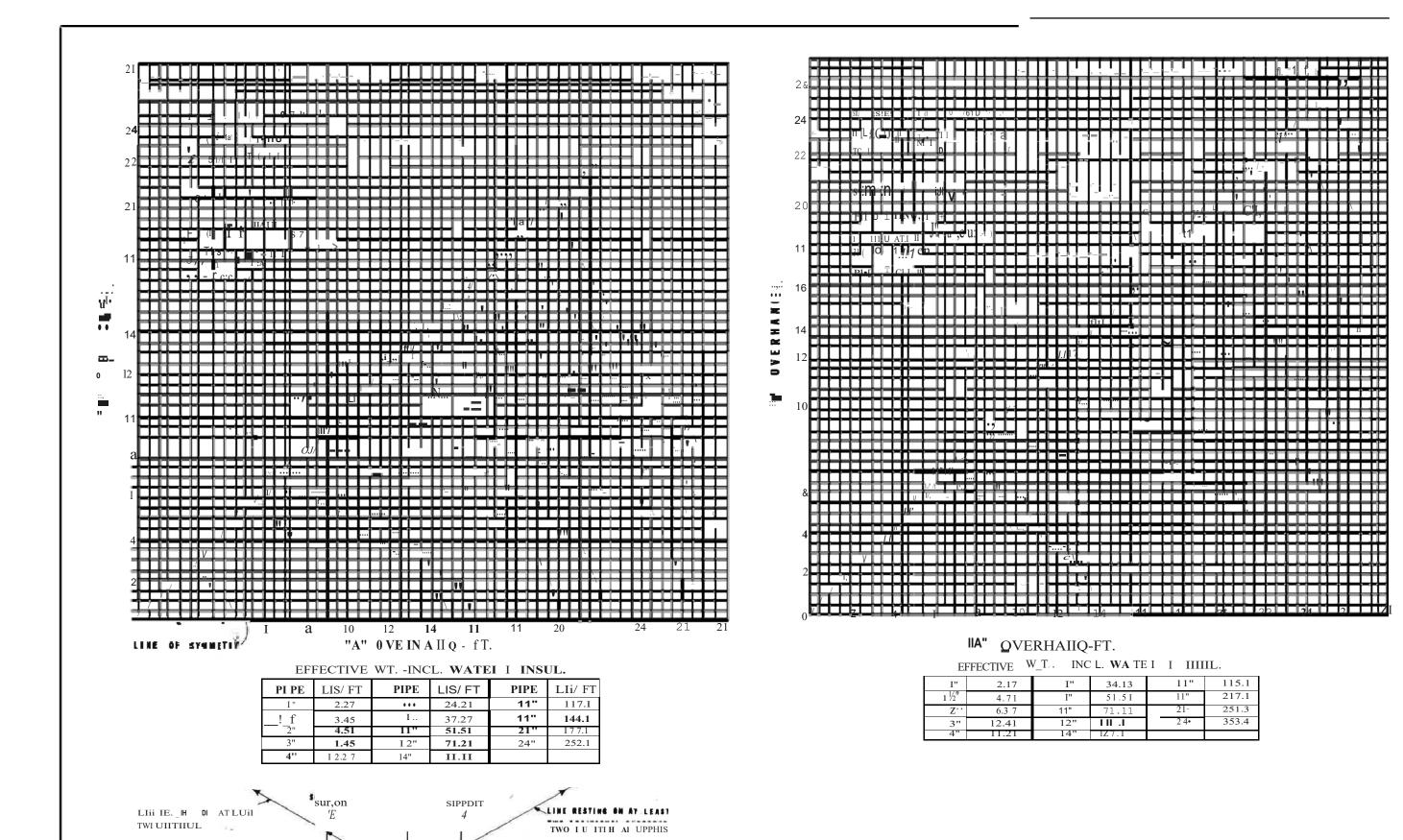
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