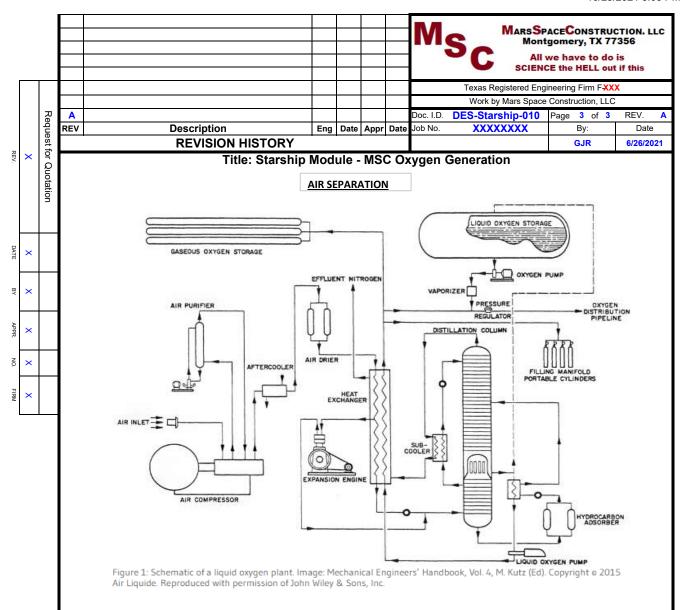
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		Air Separation This article, written by Dr. John Weisend, was originally published in the Volume 31 Number 2 issue of Cold Facts as part of											s part of	
his series, Defining Cryogenics.													•	
			ł	Air separation is one of the largest, as well as earliest,	indu	ıstri	al an	nlicat	ions of cry	ogenics	In this prod	cess cryogeni	c	
DATE	×			temperatures are used to separate air into its constitue										
			carbon dioxide (0.3%). Trace gases such as krypton, neon, xenon and helium total far less than 1%. Water vapor can also											
ВҮ	×			be a significant fraction of air but it is removed along w	/itin Ca	arb	on al	oxide	at the star	t or the	separation	process.		
				The components of air have many applications in indu										
APPR.	×			gases is a multibillion dollar industry. Air separation is such as Air Products, Air Liquide, Linde and Praxa		rin	cipal	part	of the bus	iness c	of large ind	ustrial gas fir	ms	
Ŗ				Such as All Froducts, All Liquide, Linde and Fraze										
NO.	×			There are essentially two production models used in the			•		•					
				air and the resulting components are then shipped to o second, an air separation plant is located at the custor										
FIRM	×			steel mill or nitrogen for use in pressurizing oil fields to	incre	eas	e rec	over	y. The rema	aining g	ases not of	of direct interest to the		
		<u> </u>		customer are either sold to other customers or vented									aration	
plants are quite large, with typical capacities being thousands of tonnes per day of oxygen and nitroger											n produced.			
	Cryogenic air separation is based on the principle of rectification, which is defined in Barron as "the cascading of													
		evaporations and condensations carried out in counterflow." A simple version of this is shown in Figure 1. Air is complete and all of the water, hydrocarbons and carbon dioxide are removed. The resulting air is cooled down via heat exchange												
		colder flows of nitrogen and oxygen and then expanded via both expansion engines and valves to near the saturation												
				temperature of oxygen and nitrogen. This cold, near-si- has a higher boiling temperature than nitrogen, as the										
				portion, which flows down, becomes progressively rich	er in	ОХ	ygen.	, whil	e the gas p	ortion, v	which flows	up, becomes	•	
				progressively richer in nitrogen. The liquid oxygen at the while the gas at the top is almost pure nitrogen, with s										
				plant was designed only to produce crude oxygen and					•					
				technique exist. One of the most common uses two re	ctifica	atio	n col	umns	placed on	top of e	each other,	operating at di	fferent	
				pressures. This arrangement (known as the Linde dou oxygen and nitrogen. Additional columns can be adde-								much higher p	urity	
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The need for air separation plants to compress and move thousands of tonnes of air a day means that they require significant amounts of energy. Thus, a number of energy recovery schemes are typically used, including using the work done by the gas on the expansion engines to help power the compressors. Research on modeling and optimizing the rectification columns and heat exchangers to improve the product purity while reducing energy consumption is ongoing.

Additional details on cryogenic air separation may be found in Cryogenic Engineering, R. Barron, McGraw-Hill (1966); Separation of Gases, W. H. Isalski, Oxford University Press (1989); and "Air Separation Plant Design," D. J. Hersh and J. M. Abrado, Cryogenics (July 1977). Examples of modeling of air separation plant components include "Simulation of Multistream Plate-Fin Heat Exchangers of an Air Separation Unit," R. Boehme et al., Cryogenics 43 (2003) and "Hybrid Model of Structured Packing Column for Cryogenic Air Separation," Z. Wu et al. Proc. ICEC 24 (2013). An example of using heat recovery to reduce energy use in air separation plants is presented in "A Novel Cryogenic Air Separation Process Based on Self-Heat Recuperation," Y. Kansha et al., Separation and Purification Technology 77 (2011). The relative merits of cryogenic air separation and pressure temperature swing adsorption techniques are discussed in "Comparative Analysis of Cryogenic and PTSA Technologies for Systems of Oxygen Production," T. Banaszkiewicz et al. in Adv. Cryo. Engr. Vol 59b (2014). A description of the Air Liquide helium liquefier built in Qatar may be found in "Ras Laffan Helium Recovery Unit HeRUII Project," R. Ali Said et al., Proc ICEC 2014 (at press).

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